#### **ORIGINAL PAPER**



# Evaluation of Oxidative Species in Gaseous and Liquid Phase Generated by Mini-Gliding Arc Discharge

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#### Abstract

The gliding arc discharge plasma reactors are known as a source of non-equilibrium plasma at atmospheric pressure. In the present study, generation of dominant reactive oxygen and nitrogen species in gaseous and liquid phase in water by the compact gliding arc device (mini-GAD) and corresponding bactericidal effects were investigated. Water and phosphate buffer solutions were used as model liquids. Mini-GAD is a strong source of nitrogen oxides (up to 800 ppm NO and 200 ppm NO<sub>2</sub>) that result in high concentrations of nitrites and nitrates in water solutions. The highest bactericidal efficacy towards *Escherichia coli* was achieved for non-buffered water solution.

**Keywords** Atmospheric pressure plasma · Gliding arc discharge · Plasma activated medium/water · Bactericidal decontamination

#### Introduction

Electrical discharges effecting the generation of plasma activated media (PAM)/plasma activated water (PAW) via non-thermal plasma formation are considered to be a relatively energy efficient method for production of active species. Plasma methods effectively combine the contributions of high electric fields, UV radiation and active chemicals, leading to higher treatment efficiencies. Different designs of plasma reactors and variety of electrical discharge types (AC, DC, pulsed) generated either directly in water, in the gas introduced to water or above the water surface have been studied world-wide as possible methods for abatement of chemical and biological pollutants and for generation of PAM for further use for various applications in medicine, agriculture and biotechnology [1, 2].

The gliding arc (GA) is an electrical discharge formed between two or more divergent electrodes connected to a high voltage supply with high-velocity gas flow between the

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electrodes. The arc moves from the ignition zone along the electrodes until power system is not able to compensate losses resulting from the increasing volume of plasma. Then the arc extinguishes and is rebuilt again in the ignition zone. The first applications of the GA were described by Czernichowski and included flame overheating, air depollution from volatile hazardous compounds and initiations of various chemical processes [3]. Since then, many studies have been performed on the diagnostics and the applications for purification and production of selected chemical compounds. In recent years, there have also been many publications on the use of GA in low-temperature applications due to its potential to produce a non-equilibrium plasma at atmospheric pressure [2, 4-13]. Du and Yan used GA with a mixture of distilled water and air to sterilize the isolated Escherichia coli, emphasizing the important role of the distance between the reactor and the sample [14]. Dasan et al. [15] decontaminated microbial residues from selected surfaces. Kim et al. used GA water reactor in conjunction with micro bubble generators and achieved a 6 logs reduction of colony-forming units of E. coli after 25 min of plasma treatment. The authors indicate that a high degree of oxidation was obtained due to the high content H<sub>2</sub>O<sub>2</sub> combined with lowpH acidic water [16]. Studies carried out by Kamgang-Youbi et al. shows that GA allowed to obtain activated water containing large amounts of nitrites NO<sub>2</sub><sup>-</sup>, hydrogen peroxide H<sub>2</sub>O<sub>2</sub> and peroxynitrite ONOO<sup>-</sup> after 5 min of treatment with air. The activated species acting at acidic pH showed their destructive effects on the external walls of the Staphylococcus epidermidis, Leuconostoc mesenteroides, Hafnia alvei and Saccharomyces cerevisiae and led to a decrease of their population on stainless steel and polyethylene surfaces [17]. Khani et al. [18] have shown that plasma processing using GA in inactivation peroxidase in tomatoes allowed preserving their nutritional value and is competitive in relation to other methods such as boiling water, steam and microwave. Burlica et al. used GA reactor for activation of water, using the systems above the surface and directly immersed in water. The first one allowed for the production of large quantities of molecular H<sub>2</sub>, oxygen ions and radicals, the second produced significant H<sub>2</sub>O<sub>2</sub> [19]. Wang et al. [20] used GA to convert CO<sub>2</sub> to CO and O<sub>2</sub>, indicating that the non-equilibrium nature of the discharge allows for much higher energy efficiency compared to classic thermal method. In work of Zhu et al., plasma catalysis using rotating GA allows for high conversion of methane CH<sub>4</sub> from CO<sub>2</sub>-rich biogas [21]. Bidgoli et al. applied a pulsed reactor with an electric arc moving much faster than the gas flow to direct pyrolysis of CH<sub>4</sub>. Gliding sparks produced by self-stimulated acoustic waves allow for chemical conversion rate as high as 50%, having much better performance in comparison with the conventional pulsed plasmas [22]. Several authors have also successfully used GA reactors to stimulate the growth of seeds of plants, such as wheat, *Thuringian Mallow* or hemp [23–25].

An important part of research on these applications is the investigation of corresponding plasma chemistry responsible for the formation of RONS [26–28]. Research carried out by Patil et al. shown a significant role of  $O_2$  admixtures in the formation of  $NO_x$ . For pulsed power supply, air mixtures were not only economically advantageous, but also allowed to obtain a lot of  $NO_2$  that increased with increasing  $O_2$  fraction [29]. Experiment on the sinusoidal and pulsed power supply for water spray GA carried out by Burlica and Locke has shown significant concentration of nitrates  $NO_3^-$  formed in water, when the working gases were air and  $N_2$ , compared to very low levels obtained for Ar and  $O_2$ . In case of  $O_2$ 0, it was detected only for oxygen and argon due to the decomposition of hydrogen peroxide  $O_2$ 1 by nitrite  $O_2$ 2 [30]. Porter et al. [31] reported that amount of  $O_2$ 3 is sensitive to gas carrier in case of the formation of nitrogen oxides  $O_2$ 4, which can be produced from gas mixture, ambient air and oxygen species originating from water molecules. Both groups pointed out that higher power can cause energy wasting in thermal processes and



the degradation of active species. Temperature measurements carried out by Hsieh et al. indicated the significant effect of  $O_2$  in the mixture, which increased the plasma temperature. The authors also pointed out that higher power can be related to the change in UV radiation and affecting  $H_2O_2$  production [32]. Results obtained by Wang et al. [33] indicate that  $NO_x$  production depends mainly on vibrational excitation of  $N_2$  and to a lesser extent on the thermal process. Additional information on active species in the reactor discharge chamber can be obtained using optical techniques. In the work of Sun et al., the images from the high-speed camera combined with the emission spectroscopy allowed the observation of the discharge emission and spatial distribution of species. In this case, excited  $N_2$  dominated upstream area near the electrodes, whereas downstream the main species were OH and NO [34].

The mini gliding arc discharge/device (mini-GAD) reactor is a low power consuming and compact design of the gliding arc supplied by high voltage–power supply with no separate ignition system, which can deliver certain part of the energy in the single cycle of plasma. Reactor is a portable device, designed especially for biomedical and agricultural applications and can be operated in different conditions, e.g. in various gas mixtures containing nitrogen and oxygen. It can be a good source of RONS in distant and off-grid applications. This work objective was to identify the dominant RONS generated by the mini-GAD in gaseous and liquid phases and evaluate its bactericidal effects.

# **Gliding Arc Plasma Generator**

Compact experimental set-up with mini-GAD reactor used is schematically presented in Fig. 1.

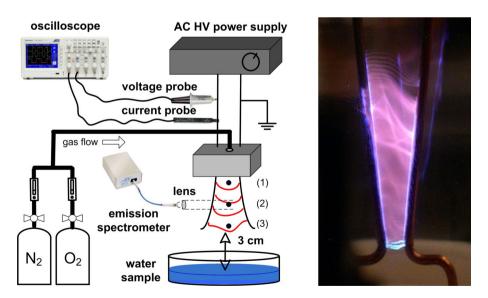


Fig. 1 Schematic diagram of the experimental setup and a photo of the discharge in mini-GAD reactor ( $N_2$ , total gas flow 7.3 l/min, camera exposure 1/60 s). Numbers (1, 2, 3) indicate the positions of measurement for emission spectra analysis



The design of the reactor was selected based on our previous experimental work [9, 15]. It consisted of two 1.5 mm thick, and 10.4 cm long copper electrodes with 12° angle between them. Inter-electrode distance in the lower part forming initial discharge gap was 3 mm. AC high-voltage-power supply of parameters enlisted in Table 1 was utilized. The power supply is based on electronic high-voltage transformer of 50 Hz operation cycle. It consists of converter giving the series of 20 kHz, high voltage irregular microimpulses in 10 ms time span so transformer works in cut-off state for the next 10 ms. It is not possible to depict a high voltage signal of 20 kHz frequency in detail with our present measuring devices. It is caused by high irregularity of the signal caused by electrical arc discharges in the gap between electrodes. Arc itself also develops in irregular way depending on the gas flow rate, type of gas, electrode geometry, material and the level of surface microcorrosion. Measurements of voltage and current waveforms of the mini-GAD were performed using a Tektronix P6015A voltage probe, Tektronix P6022 current probe and Tektronix TDS 2024B oscilloscope. Typical voltage and current characteristic are depicted in Fig. 2. The current probe was placed on the same power wire and earthed at the same point as the voltage probe. In the arc-type discharge, the current flow is mainly related to the movement of electric charges in the arc column, i.e. the conductive current. In the case of GA, the frequency was 50 Hz; the displacement currents become important at much higher frequencies. For larger distances between the electrodes when the discharge ceased, the displacement current was not possible to register with the equipment used. However, due to the fact that this factor was not taken into account, we did not to use the term of the discharge current, and the measured current values refer to the current drawn from the power supply.

During the experiments, the gas flow was directed perpendicularly to the surface of the sample (liquid) set at a distance of 3 cm from the end of electrodes. The samples were treated with GA for 2 or 5 min. Temperature of the processed gas was measured using uninsulated K-type thermocouple with electronic temperature compensation multimeter at a distance of 3 cm from the end of electrodes. It ranged from 46 to 53 °C in dependence on the gas composition and the treatment time. The temperature of treated liquids did not exceed 28 °C.

#### Results and Discussion

#### **Generation of Reactive Species in Gaseous Phase**

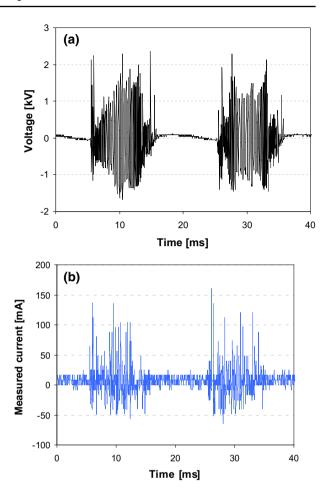
Nitrogen and oxygen based gaseous products (NO, NO<sub>2</sub>, O<sub>3</sub>) generated by mini-GAD in atmospheric pressure N<sub>2</sub>/O<sub>2</sub> mixtures in dependence on the molecular composition of feed gas were measured.

**Table 1** Parameters of the power supply used with mini-GAD reactor (primary and secondary side of transformer)

	Primary side	Secondary side	
Max. apparent power	52 VA	25 VA	
RMS voltage	235 V	687 V	
Maximum voltage	332 V	5040 V	
RMS current	0.16-0.21 A	24-37 mA	
Frequency	50 Hz	50 Hz	



**Fig. 2** Typical voltage (**a**) and current (**b**) characteristics of mini-GAD (N<sub>2</sub>+21% O<sub>2</sub>, total gas flow 7.3 L/min)



Mini-GAD is known as a good source for generation of relatively high concentrations of NO and NO<sub>2</sub>. Table 2 shows concentration of these two gaseous species in dependence of the initial oxygen O<sub>2</sub> concentrations in the nitrogen N<sub>2</sub> feed gas. Total gas flow rate was 7.3 L/min. The concentrations of NO<sub>2</sub>, NO, were measured using KANE Quintox electrochemical portable analyzer. In the mixture of N<sub>2</sub> + 32%O<sub>2</sub>, NO concentration increased up to 749 ppm and NO<sub>2</sub> to 195 ppm.

Table 2 Measured concentrations of gaseous NOx generated in  $N_2$ /  $O_2$  mixture

Initial O <sub>2</sub> (%)	NO (ppm)	NO <sub>2</sub> (ppm)	
0	0	0	
8	552	57	
21	710	129	
32	749	195	



According to our present investigations, concentration of produced gaseous ozone  $O_3$  was low. When the discharge was operated in ambient air, ozone concentration amounted to 0.32 ppm only in nitrogen as a substrate gas.

In order to further investigate the reactive species generated by the mini-GAD in various gas mixtures, time-integrated optical emission spectroscopy (OES) was performed. The OES technique can provide valuable information on excited atomic and molecular states. It enables us to determine the rotational, vibrational and electronic excitation temperatures of the plasma and thus the level of non-equilibrium [35–37]. The rotational temperature derived from the emission spectra of the  $N_2$  second positive system (SPS) can be also used as an indicator of gas temperature [35].

For fast recording of time-integrated spectra of a broad spectral region, a two-channel compact emission spectrometer Ocean Optics SD2000 (200–1100 nm, resolution 0.6–1.7 nm) was used. Spectra of the discharge in three different positions along the electrodes were measured—at the place of the smallest electrode gap, where the discharge ignites and starts to propagate (position 1), in the middle of the electrodes (position 2) and approximately 1 cm from the end of the electrodes (position 3, depicted in Fig. 1). The measured spectra were compared with simulated spectra produced by Specair software [35] in order to determine rotational and vibrational temperatures of emitting species.

In the UV range (Fig. 3), the second positive system of molecular nitrogen ( $N_2$  SPS) emission dominates in the spectra in all studied gas mixtures. The first positive system of nitrogen ( $N_2$  FPS) emission was also observed in all mixtures in the visible part of the spectra (Fig. 4), but here, the emission of O and N atomic lines was stronger.

The time-integrated OES study confirmed that mini-GAD generates highly reactive non-equilibrium plasma, since the rotational temperature  $T_r$  derived from the  $N_2$  SPS spectra (ranging from 650 to 2500 K depending on the mixture and the measurement position) was always much lower than the corresponding vibrational temperature ( $T_v$ =3500–5500 K). Figure 5 shows that in all mixtures, the  $T_r$  was the lowest in the position 1 (beginning of the discharge propagation) and the highest in the position 3 (end of the propagation). The opposite trend was observed in case of  $T_v$  (data not shown), though the changes were less significant. These results thus indicate that the

Fig. 3 The emission spectra of mini-GAD generated in mixture of  $N_2 + 21\%$  O<sub>2</sub> measured at position 2 (middle of the discharge propagation). The simulated spectra were obtained using Specair software. The  $N_2$  SPS emission shown on the figure was calculated with  $T_r = 2200$  K and  $T_v = 4500$  K

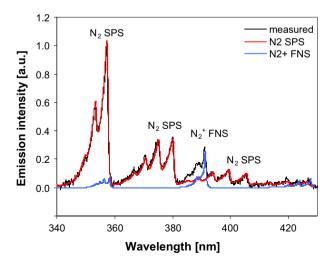




Fig. 4 The emission spectra of mini-GAD generated in mixture of  $N_2 + 21\%$   $O_2$  measured at position 2 (middle of the discharge propagation). The simulated spectra were obtained using Specair software. The N2 FPS emission shown on the figure was calculated with  $T_r = 1500 \text{ K}$ and  $T_v = 6000$  K. The emission spectra of atomic lines were simulated using electronic temperature 35,000 K, which could be much different from the real electron temperature in the plasma

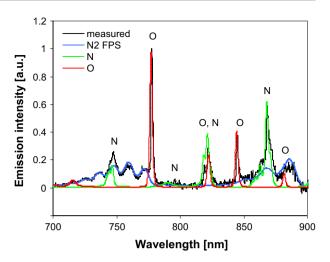
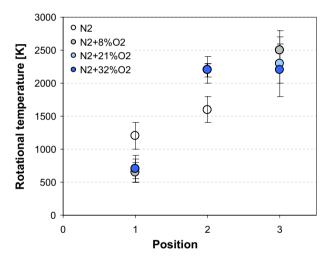


Fig. 5 The evolution of rotational temperature along the propagation of the mini-GAD in all studied gas mixtures. The rotational temperature was derived from the emission spectra of N<sub>2</sub> SPS. The position (x-axis) indicates the place between the electrodes, where the emission spectra was measured (refers to Fig. 1)



plasma generated by mini-GAD gradually approaches the thermal equilibrium during its propagation, but this equilibrium is never reached.

Figure 5 also indicates that the temperature evolution depends on the gas composition. There are several other possible mechanisms that could change the evolution of  $T_r$  and  $T_g$  in various gas mixtures. Admixtures in  $N_2$  gas can introduce new heating mechanisms [38, 39], or faster transfer of energy stored in  $N_2$  vibrational levels to the translation energy of molecules [40]. With scarce data set and with characteristic uncertainty above 100 K, we could only speculate about the real cause of the observed influence of the gas composition on estimated  $T_r$ . Moreover, we should emphasize that  $T_r$  derived from the  $N_2$  second positive emission system may not be perfectly identical to the kinetic gas temperature  $T_g$ .

On the other hand, the results of the OES (Figs. 3, 4, 5) help us to understand chemical activity of the mini-GAD. The observed emission spectra are similar to those of DC driven transient spark (TS) discharge [36]. In transient spark, the atomic lines dominate also in the visible part of the emission spectrum, whereas in the streamer corona the  $N_2$  FPS system



dominates and the emission of the atomic lines is weak. The TS is initiated by the streamer that leads to the formation of short (~10 ns) high current (~A) spark pulse [41]. The time-resolved OES study and imaging of the TS revealed that the emission from the excited molecular nitrogen is generated mostly during the streamer phase, and the emission of the atomic lines comes mainly from the spark phase [42, 43]. During the TS spark phase the heating of the gas up to 2000–3000 K was also observed, high electron density (= high degree of ionization) [44], and high degree of atomization [45]. We assume that the plasma generated by mini-GAD has similar chemical activity as the plasma generated during the spark phase of the TS discharge. This assumption is based not only on the similarity of observed emission spectra but also on fact that in both discharges, the nitrogen oxides NOx are dominant gas phase products, while the generation of O<sub>3</sub> is negligible.

High density of atomic N and O (based on strong emission of atomic lines, Fig. 4) and increase of the temperature up to ~2000 K (Fig. 5) can explain the dominant NOx formation. Under these conditions, the NO species are generated probably mainly via Zeldovich mechanism (Eqs. 1 and 2):

$$N + O_2 \rightarrow NO + O \tag{1}$$

$$O + N_2 \to NO + N \tag{2}$$

The NO<sub>2</sub> species are generated by subsequent oxidation of NO via reaction (Eq. 3)

$$NO + O + M \rightarrow NO_2 + M \tag{3}$$

In air-like mixtures the generation of ozone (Eq. 4) is possible, however here it is strongly suppressed by increased gas temperature.

$$O + O_2 + M \rightarrow O_3 + M \tag{4}$$

Further details on the air plasma chemistry leading to NOx formation in the transient spark discharge can be found in [1, 2, 46].

# **Generation of Reactive Species in Aqueous Phase**

Deionized water (DI) (<3  $\mu$ S/cm, pH $\sim$ 5.5), synthetic tap-like water (W) (8.5 mM NaH<sub>2</sub>PO<sub>4</sub> phosphate solution, $\sim$ 600  $\mu$ S/cm, pH $\sim$ 5.5) designated to mimic the natural conductivity of tap water and a weak phosphate buffered solution (PB) (2 mM Na<sub>2</sub>HPO<sub>4</sub>/ KH<sub>2</sub>PO<sub>4</sub>, $\sim$ 550  $\mu$ S/cm, pH $\sim$ 7) represent the liquid samples treated by mini-GAD. In PB solution, the range of pH was adequately buffered close to physiological pH value; providing nearly the same initial conductivities as in synthetic tap water. The initial temperature of all solutions was ambient.

In all analyzed cases, the oxidants measurement results obtained with DI and W were similar so only the results obtained with W, which actually simulate real conditions are presented in the following figures.

In the experiment, 3 mL of liquid sample was placed in 5 cm Petri dish located in a position of 3 cm from the electrodes' tips to the water surface and treated for 2 or 5 min with mini-GAD plasma. The treatment times were selected based upon our previous results on seeds treatment using the presented device due to its chemical and biological effects. The treatment period ranging from 2 to 5 min was the most beneficial for the germination energy and germination capacity of *Lavatera thuringiaca* [23]. Conductivity and pH of treated solutions are summarized in Table 3. All systems have shown similar response,



**Table 3** Conductivity and pH of treated aqueous media (mean values ± SEM)

	$N_2$		$21\% O_2 + N_2$		$O_2$	
	2 min	5 min	2 min	5 min	2 min	5 min
Cond	uctivity (μ	S/cm)				
W	$726\pm16$	$893 \pm 20$	$732\pm39$	$893 \pm 27$	$694 \pm 19$	$660\pm39$
PB	$582\pm21$	$755 \pm 13$	$548 \pm 22$	$661 \pm 53$	$613\pm60$	$609 \pm 36$
pН						
W	$3.8 \pm 0.1$	$3.4\pm0.2$	$3.7 \pm 0.2$	$3.3 \pm 0.0$	$4.1\pm0.2$	$4.6 \pm 0.1$
PB	$6.2\pm0.1$	$4.8\pm0.2$	$5.9 \pm 0.4$	$4.1\pm0.2$	$6.1\pm0.4$	$6.4 \pm 0.3$

in DI and in W after plasma treatment pH dropped to about 3.3 while in PB solution it decreased only down to 4.1. In all cases conductivity increased after the plasma treatment.

Just for verification and rough evaluation, a semi quantitative measurement of dissolved ozone  $O_3$  was performed using indigo blue method with minimal detection limit 0.05–0.5 mg/L. Indigo should be decolorised by dissolved ozone. However, even without the presence of  $O_3$  indigo could have been affected by interference with other RONS present in plasma treated water, for instance via formation of OH radicals, probably formed as a decay product from peroxynitrites. More detailed discussion on the suitability of indigo blue method for  $O_3$  detection in plasma activated water can be found in [46]. Approximately 0.8 mg/L of "apparent"  $O_3$  was recorded for 5 min GA treatment in DI.

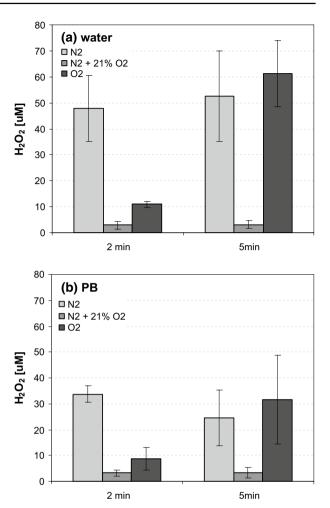
Hydrogen peroxide  $(H_2O_2)$  was measured by colorimetric method using TiOSO<sub>4</sub> (Titanium(IV) oxysulfate) solution, which reacts with  $H_2O_2$  and gives a yellow-coloured product with the absorption maximum at 407 nm. The detection limit for this method is ~5  $\mu$ M [47]. The method is independent of the pH since the measurement of  $H_2O_2$  is performed in strongly acidic solution of sulfuric acid. Due to possible  $H_2O_2$  decomposition by  $NO_2^-$  under acidic conditions, the solution of sodium azide  $NaN_3$  (60 mM) was added to the samples prior to mixing with titanium sulfate reagent to eliminate decomposition of  $H_2O_2$  [26]. The measurement results are depicted in Fig. 6. It shows that non-acidic environment of PB resulted in slightly lower concentrations of  $H_2O_2$  compared to non-buffered solutions (W, DI) where acidification occurred. The highest concentrations were obtained in the case of pure  $N_2$  and pure  $O_2$  gases, what is especially visible for 5 min plasma treatment. Low concentrations of  $H_2O_2$  in  $N_2/O_2$  gas mixture may indicate occurrence of competitive quenching reactions, most likely the reaction of  $H_2O_2$  and  $NO_2^-$  at acidic conditions leading to peroxynitrous acid ONOOH (for detailed chemistry, we refer to [1, 26, 27]).

Nitrites  $(NO_2^-)$  and nitrates  $(NO_3^-)$  were measured by the colorimetric and selective Griess assay (Nitrate/Nitrite Colorimetric Assay Kit, Cayman Chemicals). The detection limit of the assay is approximately 1  $\mu$ M for  $NO_2^-$  and 2.5  $\mu$ M for  $NO_3^-$ . This method is based on the reaction of  $NO_2^-$  with Griess reagents under acidic conditions resulting into formation of deep purple azo compound with the absorption maximum at 540 nm. Figure 7 and 8 present the concentrations of  $NO_2^-$  obtained in W and PB solutions after plasma treatment. Slightly higher concentrations of  $NO_2^-$  were achieved in non-acidic PB than W, as the acceleration of subsequent disproportionation of  $NO_2^-$  into  $NO_3^-$  occurs under acidic conditions, especially at pH below 3.5.

Nitrate NO<sub>3</sub><sup>-</sup> detection is also possible by using Griess assay, but prior to mixing of the sample with reagents, the reduction of NO<sub>3</sub><sup>-</sup> into NO<sub>2</sub><sup>-</sup> is necessary. Nitrate/Nitrite Colorimetric Assay Kit contains the nitrate reductase enzyme, which allows the NO<sub>3</sub><sup>-</sup> reduction



Fig. 6 Concentration of hydrogen peroxide  $H_2O_2$  in mini-GAD plasma treated aqueous media as function of the gas mixture. Initial values for pH and conductivity were as follows:  $pH \sim 5.5$ , conductivity  $\sim 600 \mu S/c$  m for water (W) and  $pH \sim 7$  and conductivity  $\sim 550 \mu S/c$ m for phosphate buffer (PB) solution



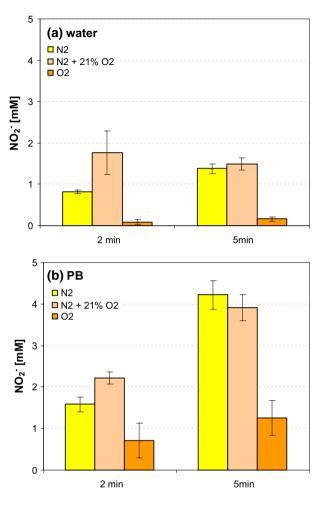
to  $NO_2^-$ . The sample after reduction gives the total  $NO_x^-$  concentration ( $NO_2^- + NO_3^-$ ) and the  $NO_3^-$  concentration can be evaluated after subtraction of  $NO_2^-$  concentration. Higher concentrations of  $NO_3^-$  after Mini-GAD treatment were detected in PB solution. Nitrites  $NO_2^-$  and nitrates  $NO_3^-$  concentrations were significantly higher when  $N_2$  was used as the substrate gas. Generated gaseous  $NO_X$  were efficiently transferred into the liquid phase adding the complexity of nitrogen oxidation cycle in liquid. Elaborated details on gasphase air plasma chemistry, the transport of species into water and subsequent liquid-phase chemistry can be found in [1].

#### **Bactericidal Effects**

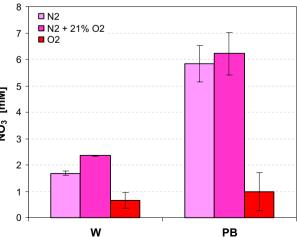
Mini-GAD was employed to reduce deposited bactericidal load on stainless steel, silicone and polyethylene terephthalate (PET) surfaces and also planktonic bacteria in the liquid media.



Fig. 7 Concentration of nitrites NO<sub>2</sub><sup>-</sup> in mini-GAD plasma treated aqueous media as function of the gas mixture



**Fig. 8** Concentration of nitrates NO<sub>3</sub><sup>-</sup> in aqueous media after 5 min treatment by mini-GAD plasma as function of the gas mixture





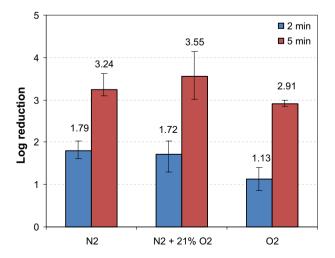
In the experiment of surface decontamination from bacteria, sterile Teflon coupons  $(15\times10\times2~\text{mm})$  were inoculated by three 10 µL droplets of Gram-negative *Escherichia coli* BW 25113 overnight culture in Miller's modified Lysogeny Broth (LB, Biolab) with initial concentration  $1.21\times10^7\pm16.1~\text{CFU/mL}$  (CFU—Colony Forming Unit). Contaminated samples were subsequently dried by gas flow from the mini-GAD and treated by GAD plasma for 2 or 5 min exposure time 3 cm from tip of its electrodes. Discharge treated samples were placed inside test tubes with 10 mL of physiological saline solution and vortexed to remove bacteria from surface to solution. Then solutions were serially diluted in 1/3 LB and plated on Petri dishes. All plates were incubated for 24 h at 35 °C, than the colonies were counted. The control samples were treated the same way except the (discharge) plasma was not turned on.

The results of this experiment are presented in Fig. 9. Log reduction (logarithmic reduction) of bacterial concentration after 2 min exposure to the mini-GAD was highest in  $N_2$ :  $1.93\pm0.23$ , similar value was in air like mixture:  $1.77\pm0.26$  and finally:  $1.11\pm0.17$  in  $O_2$ . However, these differences were not statistically significant (Kruskal–Wallis test, on the level of significance  $\alpha$ =0.05). In all three gas mixtures discharge decontamination efficiency increased significantly after 5 min exposure time. It ranged  $3.48\pm0.39$  in  $N_2$ ,  $3.62\pm0.39$  in  $N_2+21\%$   $O_2$ , and  $2.93\pm0.10$  in  $O_2$ , again these differences were not statistically significant. No thermal effects (3 cm) from mini-GAD were observed.

The results are in a good agreement with our previous findings [48]. For the case of microorganisms deposited on solid surfaces, 5 min treatment at 0.5 m³/h of N₂ flow rate resulted in reduction of *E. coli* population on stainless steel, silicone and PET surfaces about 0.91, 3.82 and 2.00 log (CFU/mL), respectively. 3.13, 3.12 and 2.55 log (CFU/mL) reductions using air were achieved on stainless steel, silicone and PET surfaces, respectively. Moreover, 5 min treatment using nitrogen resulted in reduction of Gram-positive *S. epidermis* population on stainless steel, silicone and PET surfaces about 3.60, 3.02 and 2.67 log (CFU/mL), respectively. In the case of using air, 3.28, 1.63 and 3.65 log (CFU/mL) reductions were achieved on stainless steel, silicone and PET surfaces, respectively.

For the liquid media, bactericidal effect was observed on plaktonic form of *E. coli* (CCM 394). The suspensions were prepared by the dissolution of bacteria precultivated on gelatin disc in 10 mL of desired aqueous solutions. After overnight cultivation (~18 h

Fig. 9 Log reduction of *E. coli* population on Teflon surfaces after treatment with mini-GAD in three different gas mixtures  $(N_2, N_2 + 21\% \ O_2, O_2)$  and for two exposure times (2 and 5 min). Data are represented by mean  $\pm$  SEM. Independent repeats n = 4 (n = 6 for 2 min exposure time  $N_2$  and  $N_2 + 21\% \ O_2$ )





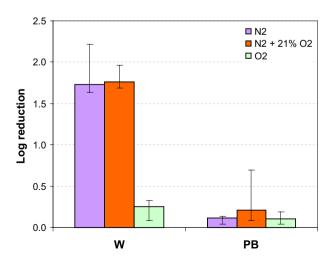
at 37 °C) were bacteria active and vital. Bacterial suspension with the initial concentrations  $\sim 10^6 - 10^7$  CFU/mL were prepared by mixing 5 mL of the overnight suspension and 45 mL of the desired aqueous solution. The number of living bacterial cells in the suspensions after mini-GAD treatment and also the control suspensions is evaluated immediately after plasma treatment by classical thermostatic cultivation on Petri dishes. The results of the bactericidal reduction are depicted in Fig. 10. Generally, relatively weak bactericidal effect was observed (<2 log for W solution).

Buffered (PB) solutions resulted in the weakest effect, as the bactericidal effect of plasma treated solutions seems to be correlated with and superposed by the decrease in pH value. In W solution the superposing of bactericidal effect is likely to be caused by peroxynitrites ONOO<sup>-</sup> or peroxynitrous acid ONOOH, and reaction between H<sub>2</sub>O<sub>2</sub> and NO<sub>2</sub><sup>-</sup>, described in detail in [1, 26, 27, 49]. Under increased acidity, decomposition reaction of peroxynitrous acid ONOOH leads to the formation of OH and NO radicals contributing to the reduction of *E. coli*. In addition to this mechanism, high NO<sub>2</sub><sup>-</sup> concentrations at acidic pH (Fig. 7a) may support the antibacterial effect of acidified nitrite, i.e. nitrous acid [26]. According to previous findings, the ionic strength of water and PB was sufficient to rule out bacteria destruction caused by osmotic stress in these solutions.

# Conclusions

We introduced and characterized a compact mini gliding arc source (mini-GAD) which is able to generate high concentrations of NOx in gaseous phase, which can be further transferred to the liquid media. The optical emission spectra characterized the GAD in various gas mixtures ( $N_2$ , air,  $N_2$ ) and enabled us to determine the typical plasma temperatures and reactive species leading to the formation of NOx. It was found that the NOx formation mechanism in GAD is similar to that in the spark phase of the transient spark discharge. Synthetic water mimicking the natural conductivity of tap water and phosphate buffer solution were used to evaluate the potential of the mini-GAD to form aqueous active species: hydrogen peroxide  $N_2$ 0, nitrites  $N_2$ 1, nitrates  $N_3$ 2 and dissolved ozone  $N_3$ 3 in water. Obtained concentrations of  $N_3$ 2 and  $N_3$ 3 were higher in the case of PB solution

Fig. 10 Bactericidal effects of mini-GAD after 5 min plasma treatment in water (W) and buffered solution (PB) as function of the gas mixture





compared with water, especially for 5 min of plasma treatment and the presence of  $N_2$  in the substrate gas. On the other hand, the highest concentration of  $H_2O_2$  was obtained in water, where the highest bactericidal activity was also observed. Mini-GAD was also demonstrated as an efficient tool for surface decontamination.

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