| 1 | Tuning composition of plasma activated water generated by   |
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| 2 | transient spark discharge with electrospray   |
| 3 |   |
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## 8 Abstract

9 Plasma-activated water (PAW) with a mixture of reactive oxygen and nitrogen species (RONS) 10 has a wide range of applications in the health, agriculture, and the food sectors. However, some 11 applications require PAW with a specific chemical composition. Therefore, we studied the generation of PAW by transient spark (TS) discharge in different gases (N<sub>2</sub>, O<sub>2</sub>, and synthetic air, 12 dry or humidified) with direct or indirect contact of the discharge with water microdroplets 13 14 formed by electrospray (ES) process. In direct contact, ES microdroplets were generated within 15 the discharge zone. In the indirect treatment, the gas was first treated by TS discharge and 16 sprayed by ES water microdroplets in the second section of the reactor. Using direct or indirect 17 treatment, different inlet gas and input energy density, PAW with different composition was 18 generated. Moreover, the obtained results allowed us to better understand the processes of PAW 19 formation. H<sub>2</sub>O<sub>2</sub>(aq) is mainly formed due to short-lived reactive species, such as the OH 20 radicals, and not by dissolution of gaseous  $H_2O_2$ . Next,  $NO_2(aq)$  ions are formed predominantly 21 by the dissolution of gaseous HNO<sub>2</sub>.

22

23 Keywords: plasma activated water, transient spark discharge, low temperature plasma,

24 electrohydrodynamic spray, nitrites, hydrogen peroxide

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# 1 **1. Introduction**

Non-thermal plasma is a flexible tool for addressing issues related to human and environmental
well-being. Cold/non-thermal plasma produces high-energy electrons that induce significant
chemical activity, making non-thermal plasma suitable for biomedical applications, water
treatment, and even air cleaning [1-5]. The reactive chemical species in the plasma can be
trapped in liquids/water to produce a chemically rich solution called plasma-activated water
(PAW) or plasma-treated liquid [6]. PAW has been extensively studied to have a wide range of
applications in food, agriculture, and biomedicine [2], [4], [6-8].

9 The high chemical reactivity of PAW can be attributed to the presence of various short- and long-

10 lived reactive oxygen and nitrogen species (RONS) [6-9]. The short-lived species produced in

11 PAW include nitric oxide (NO), superoxide  $(O_2^-)$ , ozone  $(O_3)$ , hydroxyl radical (OH),

12 peroxynitrate (OONO<sub>2</sub><sup>-</sup>) and peroxynitrite (ONOO<sup>-</sup>) with lifetimes of less than one second. The 13 long-lived species such as nitrates (NO<sub>3</sub><sup>-</sup>), nitrites (NO<sub>2</sub><sup>-</sup>) and hydrogen peroxide (H<sub>2</sub>O<sub>2</sub>) are

14 much more stable in PAW.

In a typical air plasma in contact with water, a mixture of these species is commonly produced. 15 16 However, for certain applications, only a few of these species are desirable, while others may 17 play no role or even have negative effects [10]. For example, the reactive oxidizing species 18 (ROS) such as H<sub>2</sub>O<sub>2</sub>, O<sub>3</sub>, or OH radical play important roles in bacterial inactivation, targeting cancer cells, and improving the shelf life of foods such as fruits and vegetables [11-14]. On the 19 contrary, reactive nitrogen species (RNS) such as NO<sub>3</sub><sup>-</sup> and NO<sub>2</sub><sup>-</sup> are beneficial for agricultural 20 21 applications [15-17]. ROS are important products for advanced oxidation process for wastewater 22 treatment [18], [19], instead RNS do not play a significant role in this process. Therefore, tuning 23 the composition of PAW and selective production of desired RONS in plasma-activated water is 24 very important for targeted and efficient applications of PAW [20].

25 Several authors have reported the selective production of RONS in PAW depending on the type

26 of the discharge, reactor configuration, discharge polarity or power [21-23]. It was found that

| 1  | low power (0.04-0.1 W/cm <sup>2</sup> ) surface dielectric barrier discharge (SDBD) resulted in $O_3$ as the                        |
|----|---|
| 2  | dominant species, while high power $(0.1-0.62 \text{ W/cm}^2)$ SDBD resulted in the formation of                                    |
| 3  | nitrogen oxides [21]. Positive corona, negative corona, and dielectric barrier discharge in air                                     |
| 4  | were compared for the decontamination of metolachlor pesticide and negative corona was  |
| 5  | reported to have the highest efficiency due to higher OH and H <sub>2</sub> O <sub>2</sub> concentration [22]. Machala              |
| 6  | et. al reported the dependence of the PAW composition on the discharge regime. Low power  |
| 7  | streamer corona discharge resulted mainly in the formation of H <sub>2</sub> O <sub>2</sub> and O <sub>3</sub> , while higher power |
| 8  | transient spark discharge resulted in higher concentration of $NO_3^-$ and $NO_2^-$ [23].   |
| 9  | When different gases are used, the gases dissolved in the liquid can also affect the RONS   |
| 10 | concentration in the produced PAW [24]. It was found that the presence of dissolved O <sub>2</sub> in water                         |
| 11 | favors the formation of hydroxyl radicals compared to the water with air, while $N_2$ has a certain                                 |
| 12 | promoting effect on the formation of hydroxyl radicals, nitrites, and nitrates.   |
| 13 | The chemical activity of PAW is also highly dependent on the type of interaction between the  |
| 14 | water and the plasma [25]. The transport rate of RONS from the gas to water microdroplets is  |
| 15 | faster than their transport rate to bulk water due to the increased surface area of the   |
| 16 | microdroplets [26], [27]. Numerous articles have been published on the interaction between  |
| 17 | plasma and microdroplets for bio-decontamination. For example, Ranieri et al. treated   |
| 18 | aerosolized microdroplets in a dielectric barrier discharge (DBD) reactor to decontaminate E.                                       |
| 19 | coli bacteria in a 100 L volume chamber [28]. Several researchers have chosen to treat the liquid                                   |
| 20 | in bulk and then aerosolize or electrospray the treated liquid to decontaminate small and uneven                                    |
| 21 | surfaces [29], [30].  |
| 22 | The electrohydrodynamic spray of liquids, here simply called electrospray (ES), is a simple   |
| 23 | process to generate microdroplets from a bulk liquid by means of a strong electric field [31],                                      |
| 24 | [32]. In addition to bio-decontamination, ES has a high potential in many other areas, such as                                      |
| 25 | thin film deposition [33], wet electrostatic scrubbers for submicron particle removal [34], or                                      |

26 inkjet printing systems [35].

The formation of ES microdroplets from water requires a relatively strong electric field, leading to the generation of electric discharges near the nozzle [36]. DC discharges such as corona, streamer corona, and transient spark discharge thus open the possibility of efficient production of highly reactive PAW by simultaneous generation of plasma and small microdroplets from the same high-voltage needle electrode [37-40].

6 Transient spark (TS) is a DC-driven self-pulsing discharge producing highly reactive nonthermal plasma for efficient generation of nitrogen oxides and nitrous acid [40-43]. In this work, 7 TS and ES are used in two different reactor configurations. In the first configuration, TS and ES 8 9 are generated together in the same section of the reactor. In the second configuration, the 10 discharge section and the ES section are separated, i.e. the gas is first treated by TS discharge in the first section and then sprayed by ES water microdroplets in the second section of the reactor. 11 12 In the first approach, both short-lived (OH,  $O_2^-$ , HO<sub>2</sub>, ...) and long-lived (NO<sub>2</sub>, HNO<sub>2</sub>, H<sub>2</sub>O<sub>2</sub>, O<sub>3</sub>) 13 species generated in the plasma can play a role in formation of reactive species in water, while in 14 the second approach only the long-lived species can reach the zone with the water microdroplets. 15 In addition, the experiments were performed not only in dry and humidified synthetic air, but 16 also in dry and humidified N<sub>2</sub> and O<sub>2</sub> gases separately, and at different discharge powers. The 17 goal is to show how different experimental conditions can be used to tune the PAW composition by a single type of electrical discharge. 18

In this work, the concentrations of several gaseous and liquid products were measured. There are still relatively few works that sufficiently address the composition of both gaseous and liquid products in the formation of PAW [44]. The results obtained are therefore important for a better understanding of the formation mechanisms of reactive species in PAW and for assessing the role of different gas phase species in the formation of aqueous RONS. From a practical point of view, this knowledge will allow us in the future to increase energy efficiency and selectivity with respect to the desired products when generating PAW.

26

# **1 2. Materials and Methods**

2 The experiments were conducted in a modular reactor containing either one or two sections for

3 the generation of TS discharge and ES water microdroplets and a bottom section for water

4 collection. Details of the reactor are discussed in the subsection 2.1. The generation of TS

5 discharge and ES water microdroplets is explained in subsection 2.2. The analytical methods

6 used are described in subsections 2.3 and 2.4.

# 7 2.1 Reactor details

8 Figure 1 shows a simplified schematic of the experimental system with the reactor. The reactor
9 had a cylindrical geometry with an inner diameter of 35 mm, constructed using a Prusa MK3S+
10 3D printer and using ABS (acrylonitrile butadiene styrene, a melting temperature between 22011 245 °C, high mechanical strength) and PLA (polylactic acid, a melting temperature between 17012 180 °C, very low deformability) as filament materials.



*Figure 1* - Simplified scheme of the experimental setup with the reactor having two sections (2SR),  $1^{st}$  section for TS generation,  $2^{nd}$  section for ES water microdroplets formation; HV - high voltage.

1 The 3D printing technology allowed us to construct a modular reactor with sections that can be 2 easily disassembled. The reactor can be used with two sections (2SR), with TS generation in the upper first section and ES microdroplets generation in the second section. Alternatively, TS 3 discharge and ES microdroplets can be generated simultaneously in the first section and the 4 second section can be removed. This configuration is referred to as a one-section reactor (1SR). 5 6 In both sections, a steel M6 screw was used as the ground electrode (cathode) and a blunt 7 stainless steel needle with an internal diameter of 0.6 mm was used as the high voltage electrode (anode). The needle was positioned opposite the M6 screw in a point-to-plane geometry. The 8 9 distance between the electrodes in the first section was 8 mm, while the distance between the 10 electrodes in the second section, which was used only to generate ES microdroplets, was 18 mm. The gas entered the reactor in the first section and flowed around the needle anode. The gas then 11 12 passed through the second section, which was used to generate ES microdroplets. Both water and 13 gas then entered the lower part of the reactor through a funnel-shaped junction. The water was 14 then collected at the bottom of the reactor, while the gas exited the reactor through a small opening in the side wall of the reactor. Any leaks in the reactor were sealed with vacuum grease. 15 16 Treated gases included dry and humidified O<sub>2</sub> (99.95% purity), dry and humidified synthetic air 17 (80% N<sub>2</sub>, 20% O<sub>2</sub>, 99.99% purity), and humidified N<sub>2</sub> (99.99% purity) from cylinders (Linde 18 Slovakia). A constant gas flow rate of 1 L/min was maintained for all experiments using a gas 19 flow meter (Aalborg Instruments & Controls, Inc., model P single flow tube rotameter). 20 Humidification was achieved by passing dry gases from the cylinders through a deionized water 21 (conductivity less than 3 µS/cm) in a bubbler. Typically, a relative humidity of 94–96% was 22 achieved, verified by a capacitive humidity sensor (Arduino).

## 23 2.2 Generation of discharge and water microdroplets

A high voltage (HV) DC power supply (Spellman SL30P300) connected to the needle electrode via series ballast resistor  $R = 4.6 \text{ M}\Omega$  was used to generate positive polarity TS discharge in the first section of the reactor. Despite the use of a DC power supply, TS is a self-pulsing discharge 1 due to the repetitive charging and discharging of the driving circuit capacitance *C*, with a typical 2 repetition frequency f = 1-10 kHz [41], [42]. During the charging of the capacitance *C*, the 3 voltage applied to the anode increases until it reaches a characteristic gas breakdown voltage  $V_{BR}$ .

4 The gas breakdown, initiated by a streamer, allows a rapid discharging of the driving circuit

5 capacitance and the formation of a short high current spark pulse.

6 The repetition frequency f of the transient spark process is given by the equation

7 
$$f = \left[ RC \times \ln\left(\frac{V_0}{V_0 - V_{BR}}\right) \right]^{-1}, \qquad (1)$$

8 where  $V_{\theta}$  is the input high voltage provided by the HV power supply.

9 The electrical characteristics of the TS discharge are measured with an HV probe (Cal Test 10 Electronics CT4028) and a current monitor (Pearson Electronics 2877), and then processed with 11 a digital oscilloscope (Tektronix TBS2104). The recorded waveforms are used to calculate an 12 average breakdown voltage  $V_{BR}$ , and the repetition frequency f of the transient spark pulses. 13 According to equation (1), the frequency increases as the input high voltage increases. The TS 14 discharge frequency can also be controlled by adjusting the average current supplied to the 15 circuit by the HV power supply, while the applied voltage is above the breakdown voltage. 16 Higher current means faster charging of the circuit capacitance and higher TS repetition frequency. The increase in f increases the input energy density  $E_d$  delivered by the transient spark 17 discharge [45]. The input energy density is an important parameter to evaluate the energy 18 19 efficiency of the formation of chemical products by TS discharge. The input energy density is the 20 energy delivered per liter of input gas and can be calculated as

21 
$$E_d = \frac{f \times E_p}{q} = P/q,$$
 (2)

22 where q is the gas flow rate and P is the deposited power.

23

1 Energy delivered to the plasma per pulse  $E_p$  can be calculated from the measured breakdown

2 voltage  $V_{BR}$ :

3 
$$E_p = \frac{1}{2} C V_{BR}^2$$
 (3)

The total capacitance of the electrical circuit used to generate the TS in this work,  $C = 66 \pm 6 \text{ pF}$ , 4 5 was estimated by fitting the measured dependence of the TS repetition frequency on  $V_0$  and  $V_{BR}$ 6 according to formula (1). In the experiments presented in this paper, the TS repetition frequency 7 was varied approximately in the range of 1-5 kHz by adjusting the average current supplied to the circuit by the HV power supply in the range of 0.7-2.5 mA. Consequently, the deposited 8 9 power was varied in the range of 2-14 W, and the input energy density was varied in the range of 10 100-800 J/L, with an uncertainty of up to 25%. The main source of uncertainty was the 11 determination of the repetition frequency and the average breakdown voltage. Therefore, several 12 long scale voltage waveforms covering several hundred breakdown events were recorded for 13 each experimental condition to minimize this uncertainty.

Precise repetition frequency could only be achieved by using different types of power supplies that generate short HV pulses at a predetermined frequency. However, the advantage of TS over discharges generated by short HV pulses is its ability to simultaneously generate plasma and water microdroplet electrospray. ES cannot be induced by short high voltage pulses applied to the needle. In TS, the electric field near the hollow needle tip is strong enough for microdroplets formation for most of the time between TS pulses [40].

To generate ES microdroplets directly in the discharge section (1SR), a deionized water (pH 5.8, conductivity  $<3 \mu$ S/cm) was continuously pumped into the reactor at a controlled flow rate of 500 µL/min through the HV needle anode in the first section of the reactor by a syringe pump (New Era NE-300). The needle was connected to the syringe pump by silicone tubing. To generate the electrospray in the second section of the reactor, the deionized water was pumped to the reactor by the syringe pump through the needle electrode in the second section of the reactor

1 (as shown in Figure 1), which was connected to a second high-voltage DC power supply

2 (Spellman Bertan 210-30R) via a 13.5 M $\Omega$  resistor. The electrospray was operated at a constant

3 voltage of 9 kV and the power needed to generate ES was approximately 0.2 W, for all

4 experiments when ES water microdroplets were generated in the second section.

# 5 2.3 Spectroscopic tools for diagnostics of plasma and gases

6 The top opening of the first section of the reactor is enclosed by a quartz window. This enables to 7 use optical emission spectroscopic technique for diagnostic of generated plasma. Time-integrated 8 emission spectra of spark discharges were recorded by a two-channel compact emission 9 spectrometer (Ocean Optics SD2000) with a 200-1100 nm range and resolution of 0.6-1.2 nm 10 over this broad spectral region. The wavelength response of the spectrometer was calibrated by 11 calibration lamp Avantes AvaLight-CAL-Mini.

12 To identify the emission lines in the spectra, the experimental spectra were compared with

13 synthetic spectra of different atoms and ions (N, N<sup>+</sup>, N<sup>++</sup>, O, O<sup>+</sup>, Fe, Fe<sup>+</sup>, ...) calculated for

14 different excitation temperatures, taking into account the line broadening by our spectrometer.

15 Required spectroscopic constants were downloaded form NIST atomic spectra database [46]. For

16 the calculation of synthetic spectra of molecular systems (NH A-X, N<sub>2</sub> SPS) we used Specair

17 software [47]. Details are given in Supplement II.

The main analytical technique used to determine the composition of the gas after treatment was UV-Vis absorption spectroscopy, which is suitable for detection of NO, NO<sub>2</sub>, O<sub>3</sub>, and HNO<sub>2</sub>. A deuterium lamp (Avantes AvaLight-D-S) was used as the light source and absorption spectra were measured with a spectrometer (Avantes AvaSpec-Mini4096CL) in the range 190-650 nm. The spectral resolution of this system is 0.5-0.7 nm. The absorption cuvette with length of 16 cm was used, with the absorption path 32 cm, achieved by using a mirror to make a double pass through the cuvette.

The concentration of RONS in the gas was obtained by fitting the measured absorption spectra
with calculated 'synthetic' spectra. The synthetic UV-Vis spectra were calculated by our own

1 script using the Beer-Lambert law and absorption cross sections downloaded from the MPI-

2 Mainz UV/VIS spectral atlas [48]. The downloaded absorption cross sections were convoluted to

3 match the spectral resolution of our spectrometer. This approach was verified by measuring NO

4 and  $NO_2$  concentrations in calibration gas mixtures (1000 ppm of NO in  $N_2$  and 1000 ppm of

5 NO<sub>2</sub> in synthetic air, Linde Slovakia).

## 6 2.4 Liquid phase diagnostic tools

Colorimetric methods were used to quantify the amounts of NO<sub>2</sub><sup>-</sup>(aq) and H<sub>2</sub>O<sub>2</sub>(aq) produced in
water using the Shimadzu UV-1800 UV-Vis absorption spectrophotometer. Quantitative analysis
of NO<sub>2</sub><sup>-</sup>(aq) was performed using the Nitrate/Nitrite Colorimetric Assay Kit (#780001, Cayman
Chemicals, Ann Arbor, MI, USA), which contains ready-to-use Griess reagents. Nitrites react
with the Griess reagents, to produce a deep purple azo compound. The concentration of

12  $NO_2^{-}(aq)$  was calculated from the absorbance peak at 540 nm, using a calibration curve prepared

13 by measuring the absorbance of standard  $NO_2$  (aq) solutions.

14 The concentration of  $H_2O_2(aq)$  was determined using the titanium oxy-sulfate TiOSO<sub>4</sub> assay

15 under acidic conditions (4 g/L TiOSO<sub>4</sub> mixed in a 1:1 ratio with concentrated H<sub>2</sub>SO<sub>4</sub>) [49]. In this

16 assay, titanyl ions Ti<sup>4+</sup> react with H<sub>2</sub>O<sub>2</sub>(aq) to form a yellow colored compound known as

17 pertitanic acid H<sub>2</sub>TiO<sub>4</sub>. The intensity of the color is directly proportional to the concentration of

18  $H_2O_2(aq)$ . The concentration of  $H_2O_2(aq)$  was calculated from the absorbance peak at 407 nm,

19 using a calibration curve prepared by measuring the absorbance of standard  $H_2O_2(aq)$  solutions.

20 After the discharge treatment, the sample was immediately stabilized with 60 mM sodium azide

21 (NaN<sub>3</sub>) to prevent removal of  $H_2O_2(aq)$  by its reaction with NO<sub>2</sub> (aq) under acidic conditions.

22 Sodium azide converts  $NO_2^{-}(aq)$  to molecular  $N_2$  while maintaining the  $H_2O_2(aq)$  content [50].

23 The volume ratio of sample:NaN<sub>3</sub>:TiOSO<sub>4</sub> was 10:1:5.

24 To estimate the concentration of OH(aq) radicals in treated water we used the fluorescence

25 spectroscopic technique based on the reaction of terephthalic acid (TA) with OH(aq) radicals.

26 This reaction results in the formation of hydroxyterephthalic acid (HTA). According to Mark et

1 al. [51], the vield of the TA reaction with the OH radical is 35 %. The TA solution (2 mM) was 2 dissolved in a 5 mM NaOH solution (initial pH 10) because TA is only soluble in basic solvents. Since OH radicals have a lifetime in water below 4 us [52]. TA was added to the NaOH solution 3 prior to treatment. A fluorescence spectrometer (Shimadzu RF-6000) was used to determine the 4 concentration of HTA in solution after plasma treatment, with excitation and emission 5 6 wavelengths of 310 nm and 425 nm, respectively [53]. The fluorescence intensity of the samples was compared with the fluorescence intensity of standard HTA solutions. 7 The concentration of  $NO_3^{-}(aq)$  was measured by two methods. First, an ion-selective probe 8 (Horiba LAQUAtwin NO3-11) was used. Due to cross-sensitivity, the concentration of NO<sub>2</sub><sup>-</sup>(aq) 9 10 multiplied by a factor of 0.7, as recommended by the manufacturer, had to be subtracted from the obtained apparent concentration of NO<sub>3</sub><sup>-</sup>. Second, the concentration of NO<sub>3</sub><sup>-</sup>(aq) was also 11 calculated by subtracting the concentration of  $NO_2^{-}(aq)$  from the concentration of  $NO_3^{-}$  + 12  $NO_2$ ), obtained by a colorimetric method using a reagent mixture of 10 mM 2,6-xylenol and 13 14 acids (H<sub>2</sub>SO<sub>2</sub>:H<sub>3</sub>PO<sub>4</sub> in a 1:1 ratio). The absorption maximum between 290 nm and 350 nm 15 (Shimadzu UV-1800 UV-Vis absorption spectrophotometer) is directly proportional to the 16 concentration of  $NO_x$  (aq) [54]. The concentration of  $NO_3$  (aq) was also estimated from the 17 measured pH (portable pH/ORP meter WTW 3110), assuming equilibrium conditions between  $H^+$ , NO<sub>3</sub> and NO<sub>2</sub> ions. However, due to the low repeatability, large uncertainties and in many 18 19 cases significantly different values shown by the three methods,  $NO_3^{-}(aq)$  concentrations are not reported in this paper. The amount of  $NO_3^{-}(aq)$  produced is only roughly compared to the 20 21 amount of  $NO_2^{-}(aq)$ .

22

# 23 3. Results and Discussion

The goal of the presented research is an efficient production of plasma activated water with desired composition. At the beginning of this endeavor is the ignition of the transient spark discharge and the study of its properties. Therefore, the presentation of the results starts with the description of the TS discharge behavior in the studied gas mixtures with and without water
electrospray (subsection 3.1). From a chemical point of view, the initial step in PAW production
is the generation of short-lived, highly reactive radicals and ions in the plasma. The identification
of these species by optical emission spectroscopy is described in subsection 3.2. Subsection 3.3
deals with the identification and quantification of long-lived gas-phase products. Finally,
subsection 3.4 deals with the analysis of liquid phase products.

### 7 **3.1 Electrical characteristics**

8 The electrical characteristics of TS discharge in air at atmospheric pressure are well documented 9 in our previous works [41], [42]. The electrical characteristics of TS generated simultaneously 10 with ES of water microdroplets in air have also been reported [40]. Here we therefore focus on 11 electrical characteristics of TS discharge generated in dry or humid O<sub>2</sub> and N<sub>2</sub>, with and without 12 water ES. These results are compared with the TS characteristics in synthetic air.

Figure 2a shows typical short-scale current and voltage waveforms of a transient spark discharge in humidified O<sub>2</sub> and humidified synthetic air, respectively, averaged over 128 shots, at power supply current of 1 mA. It is consistent with previously published results and confirms that TS in O<sub>2</sub> is also characterized by short high current pulses generated during the gas breakdown by rapid discharge of the total circuit capacitance [41], [42].

18 In fact, TS is based on repetitive charging and discharging of the driving circuit capacitance

19 ( $C = 66 \pm 6 \text{ pF}$ ). Figure 2b shows a series of transient spark discharges occurring simultaneously

20 with the generation of ES water microdroplets in O<sub>2</sub> (blue line) and in synthetic air (black line).

21 We have demonstrated the ability of TS and ES to coexist in synthetic air in our recent work

22 [40], where we found that TS and ES influence each other. This mutual influence causes

23 instabilities of both ES and TS. For example, the water flow required for ES causes instabilities

24 of TS, as shown in Figure 2b. There are periods of regular TS with breakdown voltage around

- 25 10 kV, but there are also periods when TS discharge is interrupted and the next breakdown and
- 26 TS spark current pulse occurs only when the applied voltage exceeds 15 kV.



**Figure 2** - Typical voltage and current waveforms of transient spark discharges in humidified  $O_2$  and in humidified synthetic air; driving circuit capacitance of  $66\pm 6 \text{ pF}$ ,  $R = 4.6 \text{ M}\Omega$ , 8 mm gap; a) short time scale with focusing on spark current pulse and voltage drop during the gas breakdown; b) long time scale voltage waveforms of TS with ES, comparison of behavior in synthetic air and in  $O_2$ .

3 Statistical analysis showed that at a power supply current of 1 mA, the TS discharge current pulses are repeated  $80\pm5$  % of the time with a relatively stable frequency of  $2.4\pm0.8$  kHz and a 4 5 breakdown voltage of 10.5±1.1 kV. Periods without TS current pulses with an anode voltage above 12 kV represent about 20% of the time. 6 7 A different behavior was observed when TS discharges with ES microdroplets were generated in 8 O<sub>2</sub> (Figure 2b, blue line). The breakdown voltage of TS with ES increased compared to the 9 breakdown voltage without ES, from 11.9±0.4 kV to 13.6±0.6 kV (power supply current of 10 1 mA), but there are not such long periods without TS pulses and with anode voltage increasing 11 up to 16 kV as in the synthetic air. The discharge characteristics in humidified N<sub>2</sub> gas are similar to those in the synthetic air. 12 13 However, in humidified nitrogen, the TS discharge is more prone to transition to a pulseless glow 14 discharge than in air. The recharging of the driving circuit capacitance required to increase the 15 anode voltage to reach the breakdown voltage again is only possible if the highly conductive 16 plasma channel decays after the TS spark current pulse and the current flow through the gap 17 stops. However, if the current supplied by the power supply is high enough, it can keep the

plasma channel active after the breakdown, thus preventing recharging of the driving circuit
capacitance. In this case, TS switches to the glow discharge [55]. Under present conditions, the
minimum current supplied by the HV power supply needed to sustain unstable glow discharge
periods is about 1.5 mA in humidified N<sub>2</sub>. In synthetic air, the TS discharge is still stable with a
current of 2.5 mA supplied by the HV power supply.

6 In dry N<sub>2</sub> without ES, the stable TS discharge was not observed at all and the discharge rapidly 7 switches to the pulseless glow discharge after a few TS spark current pulses. This behavior is probably due to the fact that in the absence of O<sub>2</sub> or H<sub>2</sub>O molecules, there are no electron 8 9 attachment reactions leading to the formation of negative ions  $(O^2, O_2^2, OH^2, H^2)$ . The formation 10 of negative ions in air plasmas reduces the concentration of free electrons and is an important 11 factor in the decay of the plasma after the TS current pulse. In dry N<sub>2</sub>, without the formation of 12 negative ions, the electrons are not efficiently quenched and the plasma can be maintained even 13 by glow discharge with a constant current of about 1 mA.

### 14 **3.2 Optical characteristics**

The emission spectra of the transient spark in air have already been presented in our previous works [42], [43]. As a novelty, we present here emission spectra of transient spark discharges operating in humidified N<sub>2</sub> and O<sub>2</sub> gases. Furthermore, we present here the influence of ES water microdroplets (500 µL/min) generated inside the discharge section on the optical emission spectra of the TS discharge. The current supplied by HV power supply was 1.1 mA.
Figures 3a and 3b show the normalized optical emission spectra of TS in humidified synthetic air, humidified N<sub>2</sub> and humidified O<sub>2</sub> gases in the spectral range of 200 to 515 nm and in the

22 spectral range from 600 to 900 nm, respectively. The emission spectra of TS in humidified

synthetic air in the 200-515 nm range are dominated by emission lines of  $N^+$  and  $O^+$  ions. It was

- 24 also possible to identify emission bands of the second positive system (SPS) of the molecular
- 25 nitrogen. It is likely that weak emission lines of  $N^{++}$  and  $O^{++}$  ions, as well as the NH (A-X)
- 26 emission system, are also present in the spectra (Supplement II, Figures SII-1, SII-3 and SII-5).



**Figure 3** - Normalized optical emission spectra of TS in humidified synthetic air, humidified  $O_2$  and humidified  $N_2$  gases in the spectral range from 200 to 515 nm (a); and in the spectral range from 600 to 900 nm (b).

The fact that the spectra are dominated by  $N^+$  and  $O^+$  lines indicates a high degree of ionization during the high current pulse of the transient spark discharge. The emission spectra of TS in humid synthetic air in the 600-900 nm spectral region are dominated by emission lines of N and O atoms. The emission intensity of the H<sub>a</sub> line near 656 nm is also relatively high. Several weak emission lines from N<sup>+</sup> ions are also present in this spectral region.

All of the above atomic and ionic emission lines and molecular emission bands are also present 8 9 in the emission spectra of TS generated in humidified N<sub>2</sub>. Of course, the emission lines of O and 10 O<sup>+</sup> species are much weaker than in humidified synthetic air because molecular oxygen is not present in the inlet gas. O and O<sup>+</sup> species must be produced by dissociation of water molecules. 11 For this reason, only the strongest lines of these species can be easily identified in the spectra 12 13 shown, such as the O triplet line at 777 nm in Figure 5b. No emission lines of N and N<sup>+</sup> species, 14 nor N<sub>2</sub> emission bands are found in the emission spectra of TS discharge in humidified O<sub>2</sub>. Only the emission lines of  $O, O^+$  and H species were identified. 15

16 In all gases, we also observed relatively weak emission lines of Fe and  $Fe^+$  species in the spectral

17 range of 200 to 280 nm. The presence of these emission lines can be attributed to the sputtering

18 of the stainless steel needle anode. The intensity of Fe and Fe<sup>+</sup> emission lines changed

1 significantly in spectra obtained from experiments with simultaneous generation of TS discharge

2 and ES water microdroplets.

Figure 4a shows a comparison of the optical emission spectra of TS in dry synthetic air with and
without ES microdroplets and in humidified synthetic air in the spectral range from 215 to
515 nm. Spectra are normalized to the intensity of the N<sup>+</sup> ion emission line near 500 nm. Spectra
of dry and humidified synthetic air without ES microdroplets are nearly identical, indicating no
significant effect of humidity on TS discharge characteristics.



**Figure 4** – Comparison of typical optical emission spectra of TS in dry synthetic air, dry synthetic air with ES microdroplets, and in humidified synthetic air; a) spectral range of 215-515 nm; b) spectral range of 600-900 nm.

10 The emission spectrum of TS generated with ES water microdroplets is also very similar to the

11 other two spectra, but only in the spectral region above 300 nm. Below 300 nm, the intensity of

12 Fe and Fe<sup>+</sup> lines in the spectrum of TS with ES increased significantly compared to the spectra of

13 TS without ES. There are probably also emission lines of Cr, Cr<sup>+</sup>, Ni and Ni<sup>+</sup> species.

14 Figure 4b shows a comparison of the optical emission spectra of TS in dry synthetic air without

- 15 and with ES microdroplets, and in humidified synthetic air in the spectral range from 600 to
- 16 900 nm. All spectra are normalized relative to the atomic oxygen triplet line near 777 nm, which
- 17 was the strongest emission line in all three spectra. All three normalized spectra shown in

Figure 4b are nearly identical, the only exception being the intensity of the  $H_{\alpha}$  line at 656 nm. The  $H_{\alpha}$  line is absent in dry synthetic air. It is only present in air with water vapor or water microdroplets. Interestingly, the relative  $H_{\alpha}$  line intensity is more than doubled in the spectrum of TS with ES microdroplets compared to the spectrum of TS in humidified synthetic air. The same differences between the spectra of TS with and without ES water microdroplets were observed when we used N<sub>2</sub> or O<sub>2</sub> gases.

The increase in  $H_{\alpha}$  line intensity in the spectra of TS with ES microdroplets compared to the spectra of TS without ES in humidified gases is potentially interesting for plasma-activated water generation. The presence of the  $H_{\alpha}$  line is mainly attributed to the impact of electrons on  $H_2O$ molecules [56]. Therefore, the increased  $H_{\alpha}$  line intensity suggests that more  $H_2O$  molecules are dissociated into highly reactive H and OH radicals in TS with ES water microdroplets compared to TS in humidified gases. In a next step, OH radicals may dissolve in the water microdroplets where they can potentially form other reactive species such as  $H_2O_2$ .

The higher intensity of Fe and Fe<sup>+</sup> (and probably Cr/Cr<sup>+</sup>, and Ni/Ni<sup>+</sup>) lines indicates increased
sputtering of the electrodes due to the presence of water flowing through the needle electrode.
For this reason, we compared the damage to the needle anode after one hour of TS operation
with and without the formation of ES water microdroplets.



*Figure 5* – *The photos of the needle electrode tip; a) new electrode; b) electrode used for one hour to generate TS in dry air; c) electrode used for one hour to generate TS and ES microdroplets.* 

1 Figure 5a shows a photograph of a new stainless steel needle with an almost flat and uniform tip. Figure 5b shows the tip of the stainless steel needle after one hour of TS discharge generation 2 (1.3 mA supplied by the HV power supply). The current pulses in TS are short enough to avoid 3 thermalization of the generated plasma, but the temperature is temporarily elevated above 2000 4 5 K during the short pulse phase [42]. This causes microscopic damage to the tip of the HV needle electrode. After one hour of operation, the burn marks with sharp edges are visible at the tip of 6 7 the anode. Figure 5c shows a tip of the needle electrode after one hour of simultaneous generation of TS (1.3 mA supplied by the HV power supply) with ES water microdroplets at a 8 9 water flow rate of 500 µl/min. A different type of erosion can be seen in Figure 5c. The electrode 10 tip is smoothed by the action of the flowing water and there are no burn marks with sharp edges. 11 The stronger intensity of the emission lines of metallic species in the emission spectra of TS with 12 ES and smoothed edges indicates that the electrospray of water facilitates and enhances the 13 sputtering of material from the tip of the anode.

14 The increased content of iron ions in the water can play an important role in the formation of the 15 plasma activated water by TS in combination with ES water microdroplets. The presence of iron 16 in the water can induce Fenton reactions causing the depletion of  $H_2O_2(aq)$ . On the one hand, this 17 could limit the maximum achievable concentration and lifetime of  $H_2O_2$  in the generated PAW, 18 but it is favorable for biomedical applications. The so-called Fenton reaction is a complex set of 19 reactions between Fe and H<sub>2</sub>O<sub>2</sub> generating both hydroxyl radicals and higher oxidation states of 20 the iron, which are capable of oxidizing a wide range of substrates and causing biological 21 damage [57].

## 22 **3.3 Gas phase products**

Optical emission spectra of TS in studied gas mixtures show production of various reactive
atoms and ions in plasma. These atoms and ions initiate a rich set of reactions that can lead to the
formation of various gaseous products (NO, NO<sub>2</sub>, HNO<sub>2</sub>, HNO<sub>3</sub>, N<sub>2</sub>O, N<sub>2</sub>O<sub>5</sub>, O<sub>3</sub>, H<sub>2</sub>O<sub>2</sub>, ...). For

1 simplicity, let's start with description of gaseous products in experiments with dry O<sub>2</sub>, where we

2 can neglect species containing H and N atoms.

Ozone is the dominant long-lived gaseous product produced by TS discharge in dry O<sub>2</sub>. It can be
produced by reaction (4)

$$5 \qquad O + O_2 + O_2 \rightarrow O_3 + O_2 \tag{4}$$

6 The formation of O<sub>3</sub> molecules most probably does not occur directly in the hot plasma filament
7 generated by the spark current pulse due to the ozone thermal instability in hot discharge
8 filaments [58]. The ozone is probably formed after the gas from the plasma channel containing O
9 atoms is mixed with the surrounding colder gas containing O<sub>2</sub> molecules.



**Figure 6** – Concentrations of gaseous products in the outlet gas as functions of the input energy density  $E_d$ ;  $O_3$  generated in dry and humidified  $O_2$ ,  $NO_2$  and  $HNO_2$  generated in dry and humidified synthetic air.

Figure 6 shows the O<sub>3</sub> concentration in the treated gas as a function of the input energy density  $E_d$ . The O<sub>3</sub> concentration initially increases to about 300 ppm at  $E_d \approx 400$  J/L. Further increase of the input energy density leads to decrease of the ozone concentration. This can be attributed to the increasing temperature of the treated gas with the increasing input energy density and the thermal instability of the O<sub>3</sub> molecules. A different trend was observed when humidified O<sub>2</sub> was treated by TS discharge. A constant O<sub>3</sub>
concentration of about 40 ppm was achieved, independent on the input energy density. This
shows that water has dominant influence on O<sub>3</sub> production in the humidified O<sub>2</sub>. First, OH
radicals are formed by electron impact dissociation of H<sub>2</sub>O molecules by reaction (5) and by
reaction with O(<sup>1</sup>D) species (6) [59], [60]:

$$6 \qquad e + H_2O \rightarrow e + OH + H, \tag{5}$$

7 
$$O(^{1}D) + H_{2}O \rightarrow OH + OH.$$
 (6)

8 Next, OH radicals can initiate decomposition of  $O_3$  by reactions (7) and (8) [61]:

9 
$$OH + O_3 \rightarrow HO_2 + O_2,$$
 (7)

$$10 \qquad HO_2 + O_3 \rightarrow OH + 2O_2. \tag{8}$$

The presence of OH radicals is important for the formation of H<sub>2</sub>O<sub>2</sub> in the treated gases, for
example by reaction (9) [62]:

13 
$$OH + OH + M \rightarrow H_2O_2 + M.$$
 (9)

14 Unfortunately, it is not possible to identify H<sub>2</sub>O<sub>2</sub> in the UV-Vis absorption spectra. In order to 15 estimate the concentration of H<sub>2</sub>O<sub>2</sub> generated in the gas phase we therefore performed several 16 measurements in which we placed a second bubbler with a de-ionized water at the outlet of the 17 reactor. The solubility of  $H_2O_2$  is so high that we can assume that practically all the  $H_2O_2$ 18 molecules produced by TS in humidified O<sub>2</sub> inside the reactor will dissolve in the water in the 19 bubbler at the outlet. After 20 minutes of accumulation, we measured the concentration of 20  $H_2O_2(aq)$  in the water, and from the amount of dissolved  $H_2O_2$  molecules we estimated the 21 concentration of  $H_2O_2$  in the gas leaving the reactor. We found that the concentration of  $H_2O_2$  in 22 the gas phase is only around 1-3 ppm.

In humid synthetic air, the concentration of  $O_3$  at the outlet is negligible. The produced  $O_3$  is consumed by reactions (7), (8), and by reaction (10) with NO:

$$25 \qquad \text{NO} + \text{O}_3 \rightarrow \text{NO}_2 + \text{O}_2. \tag{10}$$

1 Reaction (10) is so important that ozone is not detected at the outlet even in dry air, because the 2 NO concentration in the synthetic air treated by TS discharge is very high. The concentration of NO increases with increasing input energy and it can exceed 1000 ppm at about 350 J/L [45]. 3 The rate coefficient of the reaction (10) at 300 K is about  $2 \times 10^{-14}$  cm<sup>3</sup>.s<sup>-1</sup> [63]. Assuming that O<sub>3</sub> 4 is removed only by reaction (10) and there is a surplus of NO, at a constant concentration of 5 6 1000 ppm, the  $O_3$  concentration should decrease exponentially with a characteristic decay time 7 of about 2 ms. Thus, only a negligible amount of  $O_3$  can reach cuvette where the treated gas is analyzed by UV-Vis absorption spectroscopic technique. Only when the input energy density is 8 9 below ~100 J/L, the amount of NO produced is not sufficient to remove all O<sub>3</sub> molecules and 10 some of them (<10 ppm) can remain in the air treated by TS discharge [45]. 11 Despite being the dominant gas phase product, the solubility of nitric oxide is very low and NO 12 does not play an important role in the generation of PAW by TS discharge [40]. Therefore, we 13 focus here on the generation of the second and the third most abundant products,  $NO_2$  and  $HNO_2$ , 14 which are much more soluble in water than NO. Figure 6 shows the dependence of the NO<sub>2</sub> concentration in the treated gas on the input energy 15 16 density  $E_d$  in dry and humidified synthetic air. Higher amount of NO<sub>2</sub> was detected in dry 17 synthetic air than in humid synthetic air. This could be explained by the NO<sub>2</sub> generation 18 mechanism. Assuming that the majority of  $NO_2$  molecules are produced by the reaction (10), the 19 production of  $NO_2$  depends on the amount of  $O_3$  molecules produced in the treated gas. In 20 humidified air, the O<sub>3</sub> molecules are depleted by reactions (7) and (8) and fewer O<sub>3</sub> molecules 21 remain to oxidize NO to NO<sub>2</sub>. 22

Lower concentration of NO<sub>2</sub> in humid air is compensated by formation of HNO<sub>2</sub>, most likely by
the following reaction

24 
$$NO + OH + M \rightarrow HNO_2 + M.$$

21

(11)

The concentration of HNO<sub>2</sub> in humid air increases almost linearly with increasing input energy
 density and it is only by ~30% lower than the concentration of NO<sub>2</sub> in humid air (Figure 6). No
 HNO<sub>2</sub> was detected in dry synthetic air.

Although the main focus of this work is on the generation of plasma-activated water, it must be
emphasized that valuable chemical products are also generated in the gas phase during the TS
discharge. In humidified air, the TS discharge can be used as an alternative environmentally
friendly source of HNO<sub>2</sub>, with tunable concentration of HNO<sub>2</sub>, without the need for additional
valuable chemicals such as NaNO<sub>2</sub> or HCl.

### 9 **3.4 Liquid products**

For simplicity, let's start with the results of experiments using the carrier gases O<sub>2</sub> or N<sub>2</sub> (subsection 3.4.1). Without N<sub>2</sub>, the formation of reactive nitrogen species can be neglected. Without O<sub>2</sub>, reactive nitrogen species are expected to be the dominant products. When using synthetic air, we can generate PAW with a more complicated mixture of both reactive oxygen and nitrogen species, and these species may interact with each other, as discussed later in subsection 3.4.2.

### 16 <u>3.4.1 Liquid products in experiments with the carrier gases $O_2$ and $N_2$ </u>

Figure 7 compares the concentration of  $H_2O_2(aq)$  in the collected water in 1SR and 2SR reactors, with the humidified  $O_2$  and humidified  $N_2$  as inlet gases. The concentration of  $H_2O_2(aq)$  in the water from the 2SR reactor with separate TS in the first section and ES in the second section is relatively low, below 100  $\mu$ M in the case of humidified  $O_2$ . A similar concentration of  $H_2O_2(aq)$ was also detected when humidified  $N_2$  is used, not shown in Figure 7. It is reasonable to assume that the low  $H_2O_2(aq)$  concentration in the water from the reactor with two separate sections is caused by relatively small amount of  $H_2O_2(g)$  formed by TS in the first section.

24 The concentration of  $H_2O_2(aq)$  in the PAW generated in the 1SR reactor with direct contact of TS

25 discharge with ES microdroplets in the first section is significantly higher. In humidified O<sub>2</sub>, the

concentration of H<sub>2</sub>O<sub>2</sub>(aq) gradually increases with increasing input energy density up to 1 2 ~4000  $\mu$ M. In humidified N<sub>2</sub> the concentration of H<sub>2</sub>O<sub>2</sub>(aq) is lower and reaches about 1500  $\mu$ M. These results show that  $H_2O_2(aq)$  in the water in our system cannot be formed dominantly by 3 solvation of  $H_2O_2(g)$  from the gas phase, as was shown in the literature [64]. We suggest that the 4 5 formation of  $H_2O_2(aq)$  in the plasma-activated water is significantly influenced by short-lived species when water microdroplets interact directly with the TS discharge. For example,  $H_2O_2(aq)$ 6 could be produced by direct solvation of OH radicals transported into the water, where they may 7 undergo a 2-body reaction [65], [66]: 8

9

 $OH(aq) + OH(aq) \rightarrow H_2O_2(aq).$ 

(12)



**Figure** 7 - Concentration of  $H_2O_2(aq)$  as a function of input energy density; ES water flow rate 500 µl/min, duration of the experiment 2 minutes, 1SR reactor (TS and ES generated in the same section), 2SR reactor (TS in the 1<sup>st</sup> section, ES in the 2<sup>nd</sup> section of the reactor).

11 The concentration of OH(aq) in the treated water was measured to verify the possible role of OH

- 12 radicals in the formation of  $H_2O_2(aq)$ . For this purpose, terephthalic acid (TA) was used as a
- 13 fluorescent probe. TA is non-fluorescent, but readily undergoes hydroxylation upon contact with
- 14 OH radicals, producing luminescent compounds known as hydroxy-terephthalic acid (HTA).
- 15 Humidified or dry O<sub>2</sub> was used as the working gas to avoid the formation of reactive nitrogen
- 16 species. In both systems, with reactor having either one or two sections, constant liquid flow rate

of 500  $\mu$ L/min was used, and the mean input energy density was 130 ± 10 J/L. In addition, a 1 control measurement was performed to test OH(aq) radical production solely by ES in the 2 3 second section, without turning on the TS discharge in the first section of the reactor. Figure 8 shows the concentration of OH(aq) radicals as derived from the concentration of HTA 4 5 in the treated solutions. A small amount of OH(aq), was observed even in the solution from the control experiment without TS discharge, only with the formation of ES microdroplets in the 6 second section (Figure 8, column d). This could be explained by the ignition of a weak corona 7 discharge around the needle tip at an applied voltage of 9 kV, producing a small amount of OH 8 9 radicals in the gas.



**Figure 8** – Concentration of OH(aq) radicals produced in 2 mM terephthalic acid (TA) solution, a) TS and ES together in the 1<sup>st</sup> section, b,c) TS in the 1<sup>st</sup> section, ES in the 2<sup>nd</sup> section, d) no TS discharge, only ES in the 2<sup>nd</sup> section; dry (a,b) or humidified (c,d)  $O_2$ .

11 The concentration of OH(aq) radicals in the solution from the 2SR reactor experiment in dry  $O_2$ 12 at the inlet is almost the same as in the control sample (Figure 8, column b). In dry  $O_2$ , the TS 13 discharge in the first section of the reactor produces only weakly soluble  $O_3$  in the gas phase and 14 no other soluble species, e.g.  $H_2O_2$ , which could theoretically influence the formation of OH(aq)15 in the ES microdroplets in the second section of the reactor. Thus, the observed OH(aq) in 2SR

16 in dry  $O_2$  could only be produced by a weak corona accompanying the formation of ES

microdroplets. Therefore, it is reasonable to assume that the concentration of OH(aq) radicals in
the solution from the experiment in 2SR and in dry O<sub>2</sub> at the inlet should be the same as in the
control sample.

The concentration of OH(aq) is slightly higher in the solution from the experiment in the 2SR
reactor in humidified O<sub>2</sub> (Figure 8, column c). Here, the TS discharge in the first section can
produce a small amount of H<sub>2</sub>O<sub>2</sub>(g) that could be transported to the second section of the reactor.
Solvation of H<sub>2</sub>O<sub>2</sub>(g) generated by TS in the first section can explain the slightly increased
OH(aq) concentration compared to the control sample (ES without TS).

9 More important is the finding that the concentration of OH(aq) radicals is more than 4 times 10 higher in the solution from the experiment where TS and ES microdroplets interact directly with 11 each other in the first section of the reactor (Figure 8, column a). This result supports the 12 hypothesis that at least some of the  $H_2O_2(aq)$  molecules are formed from OH(aq) radicals. 13 The concentration of OH(aq) is much lower ( $\sim 10 \mu$ M) than the corresponding concentration of 14  $H_2O_2(aq)$ , ~800  $\mu$ M, obtained in 1SR reactor at an input energy density of about 100 J/L 15 (Figure 7). Note that it is not correct to compare the results obtained under different experimental 16 conditions, because the pH of the TA solution is higher than the pH of the treated deionized 17 water. However, the concentration of  $H_2O_2(aq)$  is so much higher than the concentration of 18 OH(aq) that it is very likely that some other short-lived species play a significant role in the 19 formation of  $H_2O_2(aq)$  in the system with direct contact of water microdroplets with plasma. 20  $H_2O_2(aq)$  can also be formed by a liquid phase reaction from dissolved HO<sub>2</sub> radicals [67], [68]

21 
$$HO_2(aq) + HO_2(aq) \rightarrow H_2O_2(aq) + O_2$$
,

22

23 
$$HO_2(aq) + e(aq) \rightarrow HO_2^{-}(aq),$$
 (14)

24 
$$\operatorname{HO}_{2}^{-}(\operatorname{aq}) + \operatorname{H}^{+}(\operatorname{aq}) \to \operatorname{H}_{2}\operatorname{O}_{2}(\operatorname{aq}).$$
 (15)

25

(13)

Interaction of dissolved singlet state atomic oxygen O(<sup>1</sup>D) with H<sub>2</sub>O molecules was also reported
 to form H<sub>2</sub>O<sub>2</sub>(aq) [69], [70]:

3 
$$O(^{1}D)(aq) + H_2O \rightarrow H_2O_2(aq).$$

In humidified  $N_2$ , the concentration of  $H_2O_2(aq)$  in PAW is much lower compared to the PAW 4 generated using humidified O<sub>2</sub> (Figure 7). According to Yang et al., different gases dissolved in 5 the water can affect the RONS concentration in the produced PAW, but the  $H_2O_2(aq)$ 6 7 concentration in PAW from their experiments using either water with dissolved O<sub>2</sub> or N<sub>2</sub> was the same (within the experimental error) [24]. Therefore, it is reasonable to assume that the different 8 concentration of H<sub>2</sub>O<sub>2</sub> in PAW from experiments in humidified N<sub>2</sub> and in humidified O<sub>2</sub> is not 9 10 caused by dissolved  $O_2$  and  $N_2$  itself. It is more reasonable to assume that the production of reactive oxygen species (OH,  $O(^{1}D)$ , HO<sub>2</sub>) species is lower in humidified N<sub>2</sub> than in humidified 11 12  $O_2$ , because  $O_2$  molecules cannot contribute to their formation and they can only be produced 13 from water molecules.



**Figure 9** – Influence of the input energy density on the pH evolution of PAW produced by TS and ES operated simultaneously in the first section of the rector (1SR) in humidified  $O_2$  and  $N_2$  gases.

- 15 There is another possible explanation for the lower concentration of  $H_2O_2(aq)$  in PAW from the
- 16 experiments in humidified N<sub>2</sub> compared to humidified O<sub>2</sub>. In humidified N<sub>2</sub>, NO<sub>2</sub> (aq) was
- 17 detected in most of the samples with a concentration within the ranging from 100  $\mu$ M to 450  $\mu$ M,

1 while in the humidified  $O_2$ , the concentration of  $NO_2^{-}(aq)$  was negligible. As a result, the pH of

2 PAW generated in humidified  $N_2$  decreases with increasing  $E_d$  (Figure 9).

3 Under acidic conditions, NO<sub>2</sub><sup>-</sup>(aq) can decrease the concentration of H<sub>2</sub>O<sub>2</sub>(aq) through the
4 following reactions [14], [48], [71]:

5 
$$NO_2(aq) + H_2O_2(aq) \rightarrow NO_3(aq) + H_2O_2$$
 (17)

$$6 \qquad \text{NO}_2^{-}(aq) + \text{H}^+(aq) + \text{H}_2\text{O}_2(aq) \rightarrow \text{ONOOH}(aq) + \text{H}_2\text{O}, \text{ and} \qquad (18)$$

7 
$$NO_2^{-}(aq) + H^+(aq) + 2H_2O_2(aq) \rightarrow O_2NOOH(aq) + 2H_2O.$$
 (19)

8 These reactions show that the humidified oxygen, without nitrogen, must be used for the most 9 efficient production of  $H_2O_2(aq)$ . On the other hand, these reactions show that for the production 10 of ONOOH(aq) and O<sub>2</sub>NOOH(aq), which play an important role for the antimicrobial effects of 11 water [72], it is convenient to produce a mixture of  $H_2O_2(aq)$  and  $NO_2^-(aq)$  in the liquid phase, 12 and in the gas phase we need N<sub>2</sub> in addition to O<sub>2</sub>. From this point of view, the results obtained in 13 synthetic air, which will be discussed in the next subsection, are interesting.

## 14 <u>3.4.2 Generation of plasma-activated water in synthetic air</u>

Figure 10a shows the dependence of the NO<sub>2</sub> (aq) concentration on the input energy density in water from experiments in the 2SR reactor with the first section for generation of TS discharge and the second section for ES microdroplets formation. The working gas was either dry or humidified synthetic air.

In the 2SR system, only the long-lived products generated by the TS discharge in the first section can reach the second section where they can dissolve in the ES water microdroplets. In dry air, the main gas products are NO and NO<sub>2</sub>. The formation of  $NO_2^-$ (aq) from the dissolved NO(aq) and  $NO_2$ (aq) proceeds by the following reactions

23 
$$NO(aq) + NO_2(aq) + H_2O \rightarrow 2NO_2^{-}(aq) + 2H^+,$$
 (20)

24 
$$NO_2(aq) + NO_2(aq) + H_2O \rightarrow NO_2^-(aq) + NO_3^-(aq) + 2H^+.$$
 (21)



*Figure 10* - *Influence of the input energy density (a) on the concentration of*  $NO_2^-(aq)$ , and on the pH evolution (b) of the collected water; 2SR reactor (TS in the first section, ES in the second section).

The NO<sub>2</sub> concentration generated by TS in the dry air is higher than the NO<sub>2</sub> concentration
generated by TS in the humidified air (Figures 6). On the contrary, the concentration of NO<sub>2</sub><sup>-</sup>(aq)
in water from the humidified air experiments is much higher than in the water from dry air
(Figure 10a). In humidified air, the contribution of HNO<sub>2</sub> must be taken into account:

7 
$$\operatorname{HNO}_2(\mathbf{g}) \to \operatorname{HNO}_2(\mathbf{aq}) \leftrightarrow \mathrm{H}^+ + \mathrm{NO}_2^-(\mathbf{aq}).$$
 (22)

8 Obtained results thus prove important role of HNO<sub>2</sub> on NO<sub>2</sub> (aq) formation in PAW generated by
9 TS, because the solubility of HNO<sub>2</sub> in water is much higher than the solubility of NO<sub>2</sub>.

10 The hypothesis that  $NO_2^{-}(aq)$  is formed in experiments in 2SR and humidified air dominantly by 11 reaction (22) is also supported by the finding that the concentration of  $NO_3^{-}(aq)$  in the water is 12 significantly lower than the concentration of  $NO_2^{-}(aq)$ . When dry air is used, the concentration

- 13 of  $NO_3^{-}(aq)$  is roughly the same as the concentration of  $NO_2^{-}(aq)$ , indicating the dominant role
- 14 of the reaction (21).

15 The production of  $H^+$  by reactions (20) and (21) explains the acidification of the collected water

- 16 (Figure 10b), i.e. the decrease in pH down to 2.9-3.1 with the increasing input energy density. At
- 17 low pH,  $NO_3$  (aq) is also formed from  $NO_2$  (aq) by a disproportionation reaction [49]

18 
$$3NO_2^{-}(aq) + 3H^+ \rightarrow 2NO(aq) + NO_3^{-}(aq) + H_3O^+.$$
 (23)

19 However, if the initial pH is above 3.4, the decrease of  $NO_3^{-}(aq)$  concentration is relatively slow.



*Figure 11* – *The evolution of*  $NO_2^{-}(aq)$  *concentration in the collected water from 2SR in humidified synthetic air, water flow rate 500 µl/min, experiment duration 2 minutes, initial pH*~3.4.

Figure 11 shows the evolution of the  $NO_2^{-}(aq)$  concentration in the water produced in 2SR, with 2 3 separated TS in the first section and ES in the second section, at an input energy density of about 4 220 J/l. The decrease of the  $NO_2^{-}(aq)$  concentration can be approximated by an exponential decay function with characteristic decay time of about 2200 minutes. The relatively long lifetime 5 6 of NO<sub>2</sub> (aq) can be attributed to a relatively high pH and a negligible concentration of  $H_2O_2(aq)$ in the collected water. Therefore, the disproportionation to  $NO_3^{-}(aq)$  by reaction (23) is 7 relatively slow and the conversion of  $NO_2^{-}(aq)$  by reactions (17)-(19) can be neglected. The 8 9 characteristic decay time of H<sub>2</sub>O<sub>2</sub>(aq) in PAW prepared in 1SR with O<sub>2</sub> gas with negligible concentration of  $NO_2$  (aq) is even longer, about 12000 minutes (more than 8 days). 10 The results are different when PAW is produced in the reactor where TS and ES are generated 11 12 simultaneously in the first section of the reactor (1SR). The formation of  $H_2O_2(aq)$  is not 13 negligible, because short-lived species such as OH, HO<sub>2</sub> and O(<sup>1</sup>D) radicals are likely to dissolve 14 in water microdroplets as discussed in section 3.4.1. Figure 12a shows the dependence of  $NO_2^{-}(aq)$  and  $H_2O_2(aq)$  concentrations on the input energy 15

16 density in water from the 1SR experiments in humid synthetic air. The concentration of H<sub>2</sub>O<sub>2</sub>(aq)

decreases while the concentration of NO<sub>2</sub><sup>-</sup>(aq) increases with the increasing input energy
density. We assume that the H<sub>2</sub>O<sub>2</sub>(aq) concentration decreases with increasing input energy
density due to increasing concentrations of NO and NO<sub>2</sub> in the gas. The nitrogen oxides react
with OH radicals in the gas, thus less OH radicals can be dissolved in the microdroplets, and less
H<sub>2</sub>O<sub>2</sub>(aq) is formed in the liquid phase by the reaction (12).



**Figure 12** – Influence of the input energy density on the concentration of  $H_2O_2(aq)$  and  $NO_2^{-}(aq)$  (a) and on the pH evolution (b) of the collected water; ISR (TS and ES generated simultaneously in the first section of the reactor).

- A mixture of  $NO_2^{-}(aq)$  and  $H_2O_2(aq)$  is present in PAW only when the input energy density is 8 less than 400 J/L. PAW with a relatively high concentration of both  $NO_2^{-}(aq)$  and  $H_2O_2(aq)$  (600-9 800 μM) is generated at the input energy density of 200-300 J/L. PAW generated under these 10 11 conditions can be used in applications exploiting its antibacterial properties thanks to the 12 generation of ONOOH(aq) and O<sub>2</sub>NOOH(aq) by reactions (18) and (19). Although it is still an 13 open question how to define the dose of PAW and what is the dose-response relationship of PAW 14 on cells, it was recently shown that H<sub>2</sub>O<sub>2</sub> alone and the combination of H<sub>2</sub>O<sub>2</sub> and NO<sub>2</sub><sup>-</sup> played a 15 significant role in cell death, while NO<sub>2</sub><sup>-</sup> and NO<sub>3</sub><sup>-</sup> alone had minimal effects [73]. Naturally, the mutual reactions gradually decrease the concentrations of both  $NO_2^{-}(aq)$  and 16 17  $H_2O_2(aq)$  in the generated PAW. At a pH below 3 (Figure 12b),  $NO_2(aq)$  can also be converted
- 18 to  $NO_3^{-}(aq)$  by reaction (23). The presence of  $NO_3^{-}(aq)$  in PAW immediately after the





**Figure 13** – Time evolution of  $NO_2^{-}(aq)$  and  $H_2O_2(aq)$  concentrations in PAW with an initial pH of ~2.9, TS and ES generated simultaneously in the first section of the reactor in synthetic air; input energy density ~250 J/L.

- 12 The biocidal effectiveness of PAW decreases in time due to decreasing concentrations of
- 13  $H_2O_2(aq)$  and  $NO_2(aq)$ , although it was shown that PAW can retain bactericidal effects even
- 14 after 18 months when stored at the -150 °C [74]. However, additional energy is required to freeze
- 15 PAW for longer periods. Energy efficiency is one of the drawbacks of the PAW generation
- 16 process that needs to be overcome [44], and freezing PAW would make it even worse.

1 In PAW without  $H_2O_2$ , the concentration of  $NO_2$  (aq) remains high for at least two days even at 2 laboratory temperature and an initial pH of about 3.4 (Figure 11). With pH adjusted to above 4, it 3 could probably be stored much longer in a refrigerator at 4 °C. The PAW containing mainly  $NO_2^-$ 4 without  $H_2O_2$  has no significant bactericidal effect and could not be used directly in biomedical 5 applications. However, it could be stored longer and later mixed with a solution containing an 6 appropriate concentration of  $H_2O_2$  to achieve desired dose, e.g. defined as equivalent total 7 oxidation potential [73].

In PAW from the 2SR system, with TS generation in the first section and ES in the second 8 section of the reactor, we were also able to achieve a higher concentration of  $NO_2$  (aq) than in the 9 10 1SR system with, the simultaneous generation of TS and ES in the first section of the reactor. As a result, the energy efficiency of NO<sub>2</sub><sup>-</sup> production was also better, about 2.5 nmol/J. This value is 11 comparable or even better than in some other PAW generation systems [44], [75], [76], but better 12 efficiency has also been reported [77]-[79]. For example, Xu et al. used for example low power 13 14 corona discharge (0.05 W) and achieved the energy efficiency of  $NO_2^-$  production of about 15 66 nmol/J, but with a treatment time 60 min [77]. In our system is the interaction time of water 16 microdroplets with plasma-treated humid air is very short and it can be used in continuous 17 operation mode.

18 Note that the presented work is focused on basic research and better understanding of the 19 processes behind the formation of plasma-activated water. The goal is to be able to tune the 20 composition of the generated PAW on demand. The achieved energy efficiency can be 21 significantly improved compared to the presented results in future research focused on energy 22 efficiency optimization. In addition, TS also generates other products such as NO and NO<sub>2</sub> in the 23 gas phase. These should also be taken into account, especially when considering the overall 24 energy efficiency of chemical product generation by plasma interacting with water [44]. 25 In order to improve the energy efficiency of NO<sub>2</sub><sup>-</sup> production, it would be possible to achieve it 26 by reducing the gas flow rate. If the gas flow rate is reduced from 1 l/min to 0.5 l/min. it is

1 necessary to use only 50% of the energy to maintain the same input energy density to produce 2 the same amount of HNO<sub>2</sub> in the treated gas. In this study, however, it was not desirable to reduce the gas flow rate because the TS discharge would be less stable in humidified N<sub>2</sub> and 3 would more easily switch to glow discharge. Next, it was necessary to maintain a gas flow rate 4 5 of at least 1 l/min to sufficiently flush the cuvette used to measure the gaseous product 6 concentration by UV-Vis absorption spectroscopy. Next, we could improve the energy efficiency of  $NO_2^-$  production by improving the solvation 7 efficiency of HNO<sub>2</sub> from the gas to the water microdroplets. We estimated that only about 20% 8 9 of the HNO<sub>2</sub> molecules from the gas were captured in the PAW. If all HNO<sub>2</sub> molecules were 10 used, there would be 5 times more  $NO_2^{-1}$  ions in the water, and the energy efficiency of  $NO_2^{-1}$ 11 production would increase by a factor of 5. We plan to improve the HNO<sub>2</sub> solvation efficiency by 12 tuning the ES process parameters (applied voltage, water flow rate). However, in this study, the 13 water flow rate was only 500 µL/min, i.e., the same as in the experiments in the 1SR system, 14 where TS and ES were generated simultaneously in the first section of the reactor, and the water 15 flow rate of 500  $\mu$ L/min seemed to be an optimal value taking into account the stability of the TS 16 discharge.

17

#### 18 4. Conclusions

Plasma activated water or plasma activated fluids are used in numerous applications. It is useful to study the interactions of plasmas generated by different discharges with water to understand the production mechanism of reactive oxygen and nitrogen species in PAW for tuning it for the desired applications. The use of microdroplets instead of bulk water to generate PAW increases the transport rate of reactive species from the gas to the water phase and has been reported in many studies.

In this study, PAW properties generated by transient spark discharge with direct and indirect
treatment of electrospray microdroplets are presented. Dry or humidified synthetic air, O<sub>2</sub> and N<sub>2</sub>

1 were used as working gas. For direct contact of the discharge with water microdroplets, TS and 2 ES were generated simultaneously in the same section of the reactor. As a result, PAW formation 3 was influenced by solvation of short-lived species such as OH, HO<sub>2</sub>, or O(<sup>1</sup>D) radicals. In indirect treatment experiments, the discharge was generated in the first section and water 4 5 microdroplets were generated in the second section of the reactor. Thus, the formation of PAW was only influenced by the solvation of long-lived gas species such as H<sub>2</sub>O<sub>2</sub>, NO<sub>2</sub>, or HNO<sub>2</sub>. 6 7 The comparison of results from different gases and two different reactor configurations allowed 8 us to tune the RONS compositions in PAW and helped us to understand the reaction pathways in 9 the TS-ES system. It was found that in  $O_2$ , a significantly higher concentration of  $H_2O_2(aq)$  was 10 observed in the reactor with direct contact of TS with ES water microdroplets, and it must be 11 attributed to the generation of  $H_2O_2$  in the liquid phase by short-lived species. We demonstrated 12 that the concentration of OH(aq) is much higher in PAW generated in the reactor with direct 13 contact of TS with ES microdroplets than in water from the experiments where TS discharge and 14 ES microdroplets were generated in separate sections of the reactor. However, further research is 15 needed to investigate the possible influence of other species, such as  $O(^{1}D)$  or HO<sub>2</sub> radicals, on 16 the formation of  $H_2O_2(aq)$  in PAW generated by TS in direct contact with ES microdroplets. 17 Reactor with two sections is more suitable for production of PAW with high concentration of NO<sub>2</sub> (aq). TS discharge in humidified air in the first section can produce sufficient amount of 18 19 long-lived HNO<sub>2</sub> and NO<sub>2</sub> molecules to be dissolved to ES water microdroplets in the second 20 section of the reactor. In dry air, without the formation of  $HNO_2$ , the concentration of  $NO_2^{-}(aq)$ 21 in PAW was much lower than in PAW from experiments with humidified air. This supports the hypothesis that HNO<sub>2</sub> plays a dominant role in the production of NO<sub>2</sub> (aq) in PAW generated by 22 23 TS discharge in humidified air. The advantage of using two separate sections is better stability of 24 both TS discharge and ES process. When operating together, TS discharge and ES influence each 25 other, and both discharge and ES are less regular.

In summary, it is possible to produce PAW with high concentration of  $H_2O_2(aq)$  and no  $NO_2^-(aq)$ when TS and ES are generated simultaneously in the first section of the reactor in  $O_2$ . On the other hand, PAW with high concentration of  $NO_2^-(aq)$  with negligible amount of  $H_2O_2(aq)$  can be produced by operating TS in the first section and ES in the second section of the reactor in humidified synthetic air. Both types of PAW are suitable for different applications and the selective production of either  $H_2O_2(aq)$  or  $NO_2^-(aq)$  increases the lifetime of these reactive species in PAW.

PAW with relatively high concentration of both  $H_2O_2(aq)$  and  $NO_2^-(aq)$  can be prepared in the 8 reactor with direct contact of TS discharge with ES water microdroplets in air. Reactions 9 10 between these two species reduce their lifetime to several tens of minutes, but can lead to the 11 formation of peroxynitrite, which is very important for the bactericidal effect of PAW. In the future, we plan further research focused on optimizing the formation of  $H_2O_2(aq)$  and  $NO_2^{-}(aq)$ 12 13 in a buffered solution. Keeping the pH of the treated solution above 4 could increase the lifetime of  $H_2O_2(aq)$  and  $NO_2(aq)$  while maintaining the bactericidal effects of the prepared plasma-14 15 activated solution.

16 Finally, the optical emission spectra revealed another new interesting phenomenon when TS 17 discharge is generated simultaneously with ES water microdroplets. The intensity of Fe and Fe<sup>+</sup> 18 emission lines increased significantly. In order to obtain a higher concentration and lifetime of 19  $H_2O_2(aq)$  in PAW, it is necessary to test the use of electrodes made of another metal such as 20 tungsten. On the other hand, the presence of Fe atoms in the water can induce Fenton reactions 21 causing depletion of H<sub>2</sub>O<sub>2</sub> favorable for biomedical applications. In addition, the improved 22 sputtering of steel electrodes indicates that TS generated simultaneously with ES could be used 23 for the degradation of various dyes without the addition of an external catalyst source needed to 24 initiate Fenton reactions. Therefore, additional measurements using time-resolved optical 25 emission spectroscopy are planned to better understand and optimize Fe and Fe<sup>+</sup> formation with 26 simultaneous generation of TS and ES water microdroplets.

1

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